



1 **Adsorption and Desorption studies of *Delonix regia* pods and leaves:**  
2 **Removal and recovery of Ni(II) and Cu(II) ions from aqueous solution**

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11 **Abstract**

12 In this study, the adsorption of Ni(II) and Cu(II) ions from aqueous solutions by powdered pods  
13 and leaves of *Delonix regia* was investigated by batch adsorption techniques. The effects of  
14 operating conditions such as pH, contact time, metal ions concentration and the presence of  
15 sodium ions interfering on the sorption process were investigated. The results obtained showed  
16 that the equilibrium sorption was attained within 30 min of interaction and the adsorption  
17 process followed the pseudo-second-order kinetic model for all the metal sorption with the  
18 exception of Cu(II) sorption on the leaves. The equilibrium data fitted well with both the  
19 Langmiur and Freundlich Isotherms; the desorption study revealed that the percentage of metal  
20 ions recovered from the pods were higher than the leaves at various concentration of nitric acid.  
21 This study has proven that *Delonix regia* biomass, an agro-waste could be used for removing  
22 Ni(II) and Cu(II) ions from wastewater

23 **Keywords:** *Delonix regia*, low-cost adsorbent, Ni(II) ions, Cu(II) ions, equilibrium, kinetics

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37 **1. Introduction**

38 The persistent nature, non-biodegradability, toxicity and ability of heavy metals to bio-  
39 accumulate in the environment and cause serious pollution have made heavy metals priority  
40 pollutants (Hamza et al., 2013). Various health effects are caused by anthropogenic pollutants  
41 in water; which are majorly heavy metals such as mercury, nickel, lead, cadmium copper, zinc  
42 and cobalt (Hamza et al., 2013; Singh et al., 2011). Heavy metals gain entrance into water  
43 supply by industrial activities such as electroplating, smelting, glass and ceramics, mining,  
44 textiles, storage batteries, petroleum, metal finishing, pulp and paper (Dean et al., 1972). Apart  
45 from the damage to the marine ecosystem, damage caused by copper to the marine life include  
46 damage of gills, liver, nervous system, kidneys and changing the sexual life of fishes  
47 (Flemming and Trevors, 1989; Ho et al., 2002; Van Genderen et al., 2005). Although, copper  
48 is known to play a vital role during metabolism in animal; its excessive intake can result in  
49 serious health problems (Paulino et al., 2006). Reactive free oxygen species which damage  
50 lipids, proteins and DNA are released when copper is present in the blood system (Brewer,  
51 2010). Wilson's and Alzheimer's diseases, mental illness, Indian childhood cirrhosis and  
52 schizophrenia are reported to be caused by excess copper in the blood (Brewer, 2007; Faller,  
53 2009; Hurean and Faller, 2009). Like most heavy metals, nickel has its detrimental effect on  
54 human health resulting in allergic dermatitis, immunologic urticarial; immediate and delayed  
55 hypersensitivity. All nickel compounds except for the metallic nickel have been classified as  
56 human carcinogens by the International Agency for Research on Cancer (IARC) (IARC, 1990)  
57 and the U.S. Department of Health and Human Services (DHHS, 1994).

58 Conventional methods for the treatment of metal ions includes: reverse osmosis, chemical  
59 precipitation, oxidation/reduction, ion exchange, electrochemical processes, membrane  
60 separation and evaporation. These techniques require high operational costs and yield minimal  
61 removal efficiencies, they have been reported to be expensive and inadequate. Therefore, there  
62 is the need to investigate alternative techniques that are cheaper, efficient and easy to handle.  
63 One of such techniques is biosorption, that is, the use of low-cost adsorbent like agricultural  
64 materials of no economic value and industrial by-products (Jeme, 1968; Inoue and Munemori,  
65 1979) for the removal of heavy metal ions from polluted water.

66 Almond shell tree bark treated with formaldehyde and sulphuric acid (Guibal et al., 1993; Raji  
67 et al., 1997), bone char, tea leaves, wood charcoal (Ajmal et al. 2003), coconut shell have been  
68 used to produce activated carbon to treat heavy metal ions from wastewater. Rice hulls, rice  
69 bran and pine bark (Nath et al., 1997) have also been used in the raw and treated form to remove



70 heavy metal ions. The removal of Ni(II) ions from aqueous solution using sugarcane bagasse,  
71 an agricultural waste biomass has been investigated by Garg et al. (2008). The optimum  
72 conditions for maximum removal of Ni(II) ions from an aqueous solution of 50 mg/L were  
73 reported to be adsorbent dosage of 1500 mg/L, pH 7.5 and a stirring speed of 150 rpm.  
74 Moodley et al. (2011) investigated the adsorption capacity of pine sawdust by treating  
75 wastewater containing Ni (II), and other metal ions (Co(II) and Fe(III) ions). The authors  
76 reported that the Freundlich isotherm fitted the experimental data better than the Langmuir  
77 isotherm and that the use of pine sawdust could be a promising solution to the elimination of  
78 Ni(II) ions from multi-component aqueous solutions. The adsorption and desorption of Ni(II)  
79 ions from aqueous solution by a lignocellulose/montmorillonite nanocomposite was reported  
80 by Zhang and Wang (2015). Their report indicated that the maximum adsorption capacity of  
81 Ni(II) ions reached 94.86 mg/g at an initial Ni(II) ions concentration of 0.0032 mol/L, a  
82 solution pH of 6.8, temperature of 70°C, and contact time of 40 min. Kahraman et al. (2008)  
83 examined the use of cotton stalk and apricot seed as alternative adsorbents for the removal of  
84 Pb and Cu. The treatment of Pb and Cu with these agricultural wastes was reported to reduce  
85 their toxic effects on *P. aeruginosa*. The sorption capacity of Cu(II), kinetics and isotherms of  
86 different low-cost residual agricultural materials including peanut shells, nut shells, plum  
87 seeds, eucalyptus bark, olive pips, peach stones, and pine sawdust was studied by Hansen et al.  
88 (2010). It was found that the pseudo-second-order model described the sorption kinetics  
89 satisfactorily, while, the Langmuir and Freundlich models described the equilibrium sorption  
90 isotherms well for the biosorbents. Moreover, Abdel-Tawwab et al. (2017) used rice straw,  
91 sugarcane bagasse, and maize stalks for the removal of Pb, Cd, Cu, and Zn from aqueous  
92 solution. All the biosorbents were reported to be effective and cheap for the removal of the  
93 metal ions from polluted water, with rice straw showing a higher adsorption efficiency than the  
94 others. The application of treated pumpkin husk as an excellent adsorbent for removing Cu(II)  
95 and Ni(II) ions has been reported by Samuel et al. (2016). The adsorption of Cu(II) and Ni(II)  
96 ions was found to be suitable at pH 5. The Langmuir isotherm data fitted well the equilibrium  
97 data, whereas, the kinetic experimental data correlated well with the pseudo-second-order  
98 kinetic model.

99 Therefore, the objective of this research work is to investigate the capacity of an agro-waste  
100 *Delonix regia* pods and leaves in the removal of Ni(II) and Cu(II) ions from aqueous solutions.  
101 The desorption of bound metals from spent *Delonix regia* pods and leaves using various  
102 concentrations of nitric acid was also considered. *Delonix regia* is popularly grown in Africa  
103 and Hong Kong as a shade tree and for ornamental purpose. The tree has pods that can be as



104 long as 60 cm in length and 5 cm wide, with a distinct bright green fern-like compound leaves.  
105 It belongs to the flowering plant family *Fabaceae* and commonly called the flame of the forest  
106 tree. The outcome of this research would be of great benefit to most industries in the developing  
107 countries of the world, the adsorbent would serve as cheaper adsorbent for the removal of heavy  
108 metals from wastewater.

## 109 2. Materials and methods

### 110 2.1 *Delonix regia* sample

111 Leaves and pods of *Delonix regia* collected from Ekiti State University, Ado-Ekiti, Nigeria  
112 were used as adsorbent for the sorption study. After milling, the adsorbents were sieved through  
113 a 250µm mesh nylon sieve and kept in air tight containers until required for use.

### 114 2.2 Chemicals and reagents

115 Diammonium nickel hexahydrate and copper chloride dihydrate salts supplied by Merck,  
116 Germany were dissolved in high purity milli-Q water to prepare 1000 mg/L stock solutions of  
117 Ni(II) and Cu(II) ions, respectively. Working standard solutions were prepared from the stock  
118 solutions and pH adjustment was done with 0.1 M HNO<sub>3</sub> and 0.1 M NaOH when necessary.  
119 The effect of solution ionic strength on sorption was studied using different concentrations of  
120 sodium nitrate salt and desorption of bound metal from spent biomass was achieved with  
121 different concentrations of HNO<sub>3</sub>.

### 122 2.3 Characterization

123 The elemental composition of the pods and leaves of *Delonix regia* was achieved by energy  
124 dispersive spectroscopy (EDS). The morphological study was by the scanning electron  
125 microscope (Nova Nano SEM 230) and the transmission electron microscope (FEI Tecnai G<sup>2</sup>  
126 20). X-ray diffractometer (Siemens D8 Advance Bruker XRD) was used for phase  
127 characterization.

### 128 2.4 Adsorption

129 Adsorption procedure by Meena et al. (2008) was slightly modified and use in this work. As  
130 soon as each experiment is concluded, an aliquot is withdrawn and diluted with 0.1 M HNO<sub>3</sub>  
131 before residual metal content is analysed with ICP-MS (X Series). Each experiment was carried  
132 out in triplicate and the results are the average values. The amount of Ni(II) and Cu(II) ions  
133 sorbed on the pods and leaves of *Delonix regia* ( $Q_e$ ) was calculated using Equation 1.

$$134 \quad Q_e = (C_o - C_e)V/m \quad 1$$



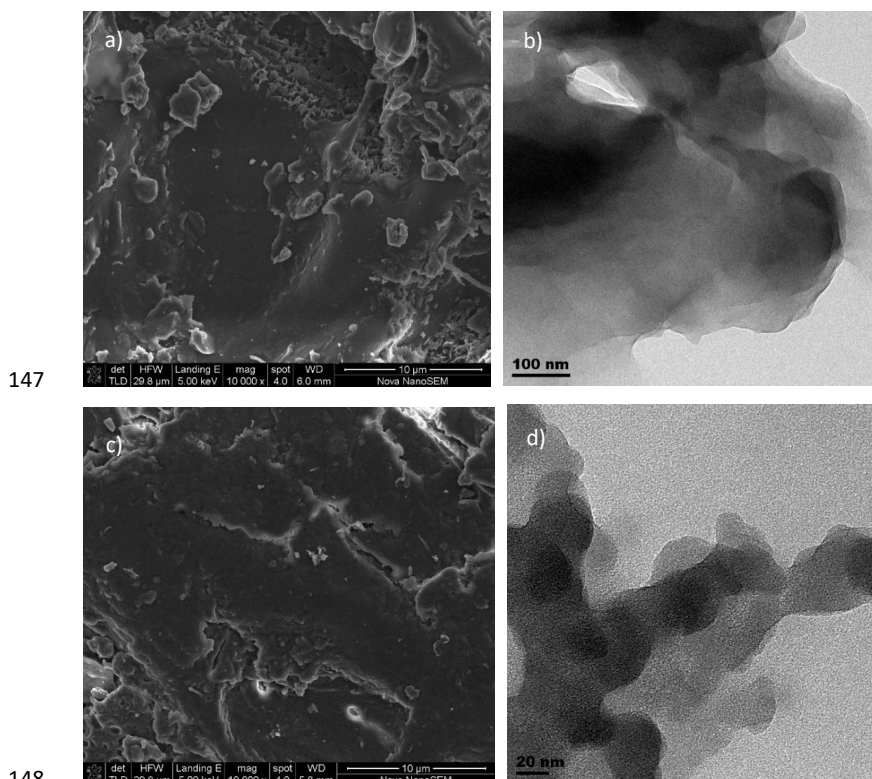
135 where  $C_0$  is the initial metal concentration (mg/L),  $C_e$  is the final metal ion concentration in the  
136 solution, ICPMS reading (mg/L),  $V$  is the volume of the metal solution used in litre (L) and  $m$   
137 is the mass of the biosorbent (g).

### 138 3. Results and discussion

#### 139 3.1 SEM-EDS, TEM and XRD analyses

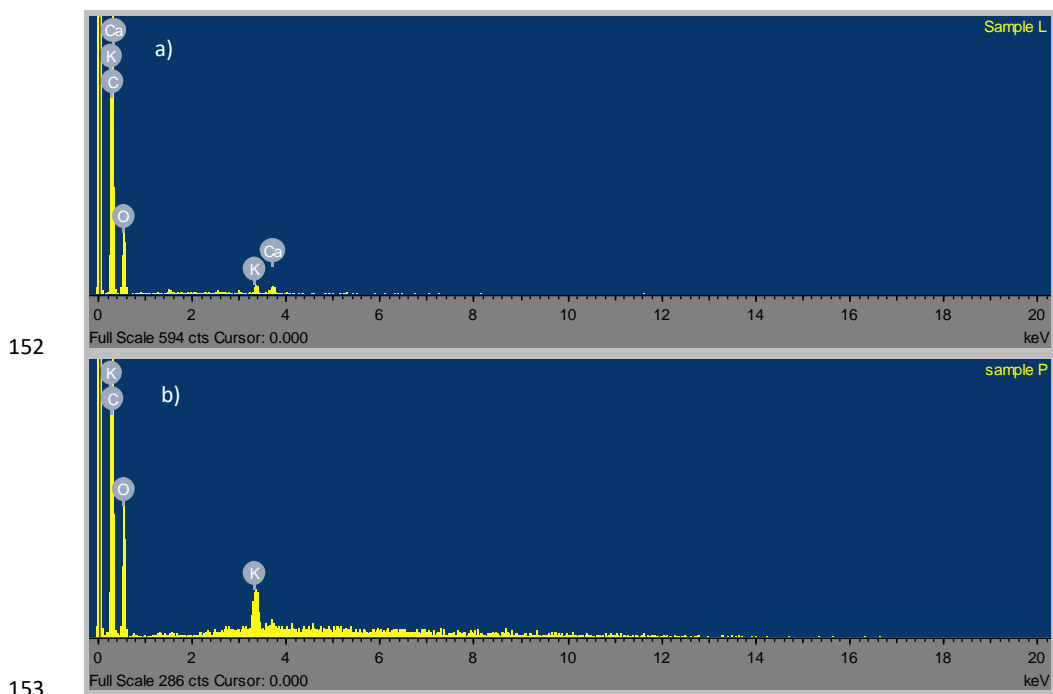
140 The SEM (at x10 000 magnification) and TEM micrographs of the pods and leaves of *Delonix*  
141 *regia* (Fig. 1) indicated the spongy nature of *Delonix regia* with porous structures. This  
142 structural properties might improve the uptake of the Ni(II) and Cu(II) ions from aqueous  
143 solution. The EDS of *Delonix regia* showed that the surfaces of the leaves is composed of  
144 66.79% C, 32.97% O and traces of Ca and K, while, the pods is composed of 57.61% C, 41.15%  
145 O and trace of K.

146



149 **Figure 1.** SEM (at x10 000 magnification) and TEM micrographs of *Delonix regia* leaves (a  
150 & b) and pods (c & d)

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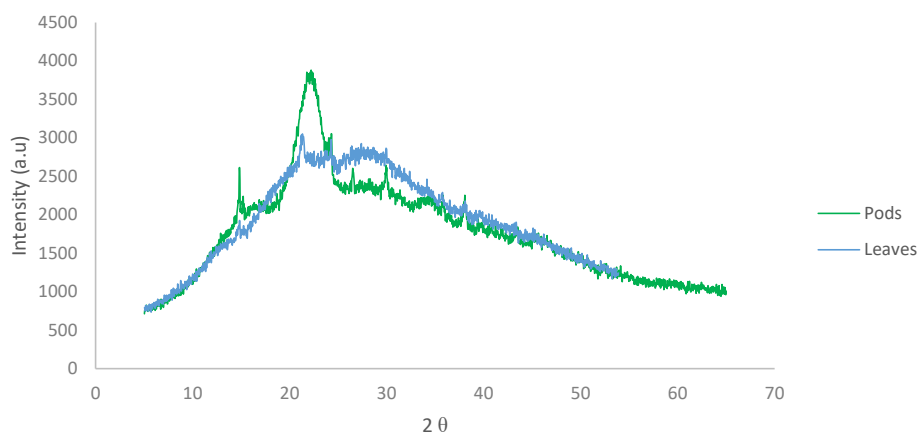
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154 **Figure 2.** EDS of leaves (a) and pods (b) of *Delonix regia*

155

156 Native cellulose ( $C_6H_{12}O_6$ )<sub>x</sub> was identified in *Delonix regia*, the peak at 22.15° for pods and  
157 21.36° for the leaves may be due to the amine, hydroxyl, aldehydic and ketonic groups of the  
158 hemicellulosic moieties. Thus, the pods and leaves are rich in cellulosic material which may  
159 provide sites for the binding of Ni(II) and Cu(II) ions.

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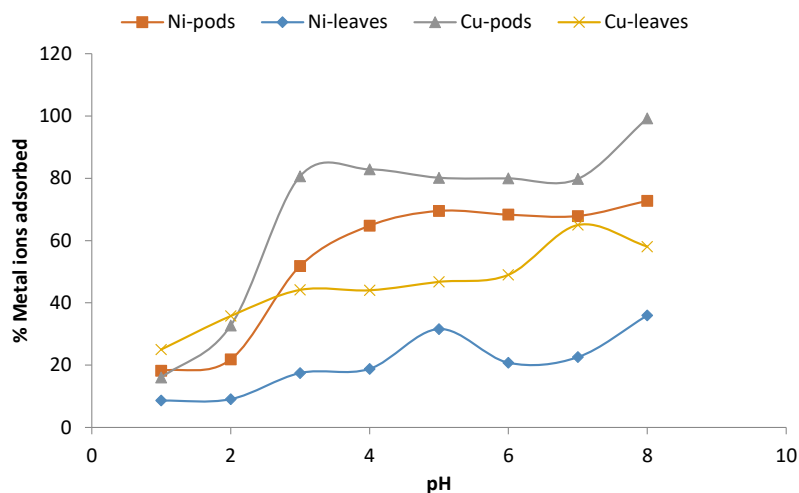
161  
162 **Figure 3.** X-ray diffractogram of the leaves and pods of *Delonix regia*

163

### 164 3.2 Adsorption studies

#### 165 3.2.1 pH

166 The result of the study of pH on the adsorption of Ni(II) and Cu(II) ions onto *Delonix regia* is  
167 shown in Fig. 4. The figure revealed that there was no significant nickel uptake by both  
168 adsorbent at low pH, but a very noticeable uptake was achieved as pH increases. This showed  
169 that the sorption of Ni(II) on *Delonix regia* pods and leaves is pH dependent. pH 5 at which  
170 maximum sorption was recorded is used as the optimum pH and used in subsequent  
171 experiments. Saeed et al. (2005) reported an optimum sorption pH of 6 for Ni(II) on crop  
172 milling waste while pH 5 was reported for its sorption onto natural neem sawdust and almond  
173 husk (Hasar, 2003; Rao et al., 2007).



174  
175 **Figure 4.** Effect of pH on the adsorption of Ni(II) and Cu(II) by *Delonix regia* pods and leaves.  
176 *Experimental conditions:* pH 1-8; contact time: 300 min; metal ions concentration: 100 mg/L

177

178 A small increase in uptake value was achieved between pH 1 to 3, but maximum uptake of  
179 46.7% was recorded at pH 5 for Cu(II) ions sorption onto leaves and maximum uptake of 82.9%  
180 at pH 4 for Cu(II) ions onto the pods. pH 4 was used for sorption experiment of Cu(II) ions to  
181 *Delonix regia* pods while pH 5 was used for adsorption of Cu(II) onto the leaves. The increase  
182 recorded at pH 6 and 7 were not considered in choosing the optimum pH at which Cu(II) ions  
183 sorption onto the leaves occurred because visible precipitate had been formed in the  
184 experimental set up at these pH. Thus, pH 5 was used for other studies. Some literatures  
185 reported pH 5 and 5.8 as the optimum for the uptake of Cu(II) ions by some modified natural  
186 wastes (Shukla and Pai, 2005; Witek-Krowiak et al., 2011; Anantha and Kota, 2016).  
187 Generally, the result pointed to the fact that enhanced metal uptake is possible by increasing  
188 the pH of the sorption media, this might be a result of the increased overall negative charge  
189 particularly between pH 4 and 6. When this happened, there is increased negative charge on  
190 the adsorbent surface; this will lead to an increasing electrostatic attraction between positive  
191 ionic species and adsorbent particles which would subsequently lead to increase sorption of  
192 metal ions. The increase of pH definitely decrease the concentration of hydrogen ions and  
193 therefore the competition between metal ions and hydrogen ions for active sites on the  
194 adsorbent is reduced. This will lead to increase sorption of metal ions to the adsorbent  
195 (Kadirvelu et al., 2000; Kadirvelu et al., 2001; Sánchez-Polo and Rivera-Utrilla, 2002;  
196 Kadirvelu et al., 2003; Meena et al., 2005).

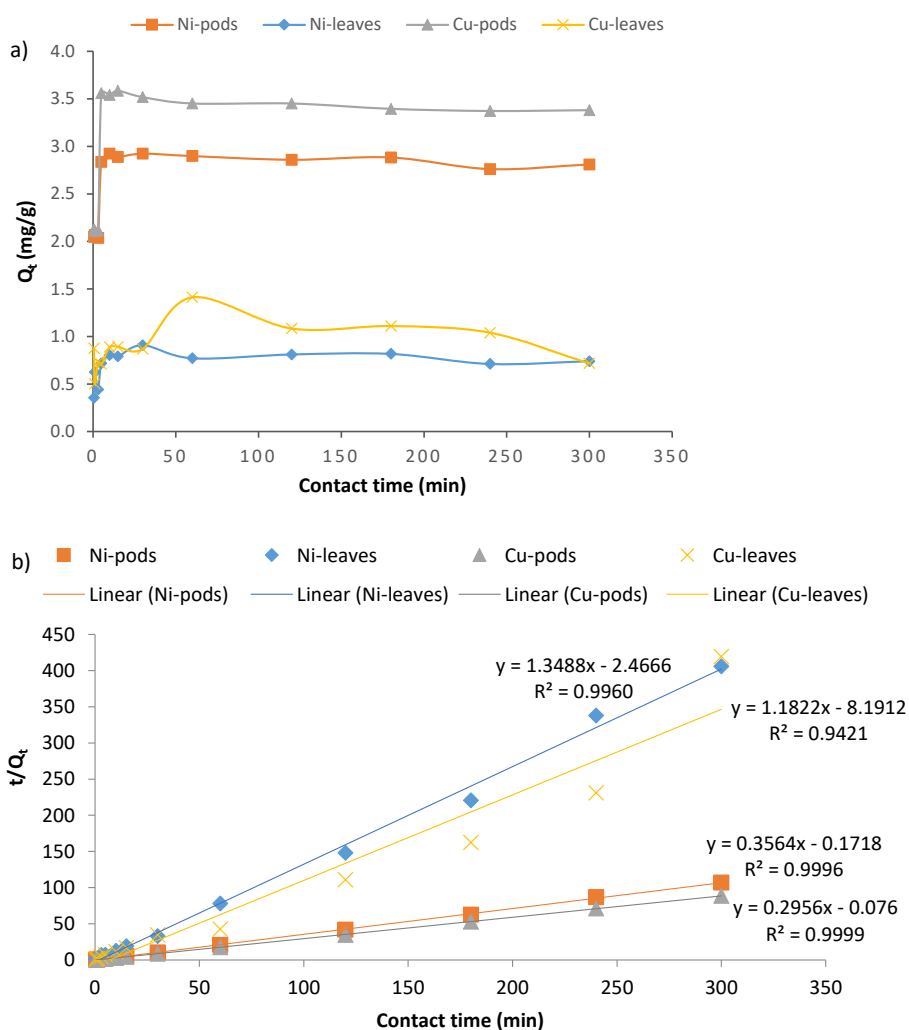




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198 3.2.2 Contact time

199 The result shown in Fig. 5a was obtained from time of agitation of the biomass and adsorbate  
 200 on an end-over-end shaker. Investigating the effect of agitation time performed at time intervals  
 201 of 5 min up to 300 min showed that the two adsorbents used in this work had rapid uptake for  
 202 the metal ions within short period of interaction.



203

204

205 **Figure 5.** Effect of contact time (a) and pseudo-second-order kinetics (b) of the adsorption of  
 206 Ni(II) and Cu(II) ions by *Delonix regia* pods and leaves. *Experimental conditions:* pH 4 and 5;  
 207 contact time: 5-300 min; metal ions concentration: 100 mg/L

208



209 A slight desorption and adsorption was observed between 5 to 10 min of interacting the  
210 adsorbent with the metal ion solution. Within 30 min of interaction, maximum uptake has been  
211 achieved on both adsorbents irrespective of the metal considered, though the uptake recorded  
212 on the pods were higher than those on the leaves. Metal uptake by the adsorbent remained fairly  
213 constant after 30 min of interaction to the end of the experiment.

214 Further examination of the contact time experiment was carried out by modelling the data with  
215 the pseudo-first-order, pseudo-second-order kinetic models and intra particle diffusion models,  
216 to determine the mechanism of the sorption process. Results obtained showed that the process  
217 was well fitted to the pseudo-second-order kinetic model. This is supported by the work of  
218 Hansen et al. (2010), the plots and kinetic parameters for this model are shown in Fig. 5b and  
219 Table 1, respectively.

220  
221 The pseudo-second-order kinetic model is a pointer to the fact that the mechanism involved in  
222 the sorption is governed by ion exchange or sharing of electrons.

223 The pseudo-second-order kinetic model is well expressed in Equation 2 where  $k_2$  (g/mg/min)  
224 represent the rate constant for the pseudo-second-order kinetics;  $Q_e$  and  $Q_t$  (both in mg/g) being  
225 the amount of adsorbate taken up by the adsorbent at equilibrium and at any time  $t$ , respectively.  
226 All parameters in Equation 2 were derived by plotting  $t/Q_t$  against  $t$ .

$$227 \quad t/Q_t = 1/k_2 + t/Q_e \quad 2$$

228 **Table 1.** Parameters obtained from the pseudo-second-order kinetic model

Metal ions	$Q_e$ (mg/g)	$k_2$ (g.mg <sup>-1</sup> min <sup>-1</sup> )	$r^2$
<i>Delonix regia</i> pods			
Ni	2.8	-2.36	0.9996
Cu	3.4	-3.24	0.9999
<i>Delonix regia</i> leaves			
Ni	0.7	-0.25	0.9960
Cu	0.8	-0.09	0.9421

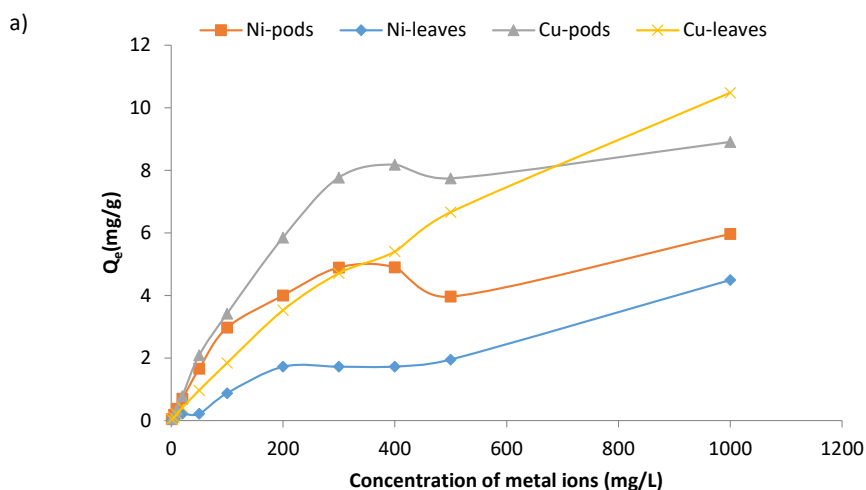
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### 230 3.2.3 Initial adsorbate concentration

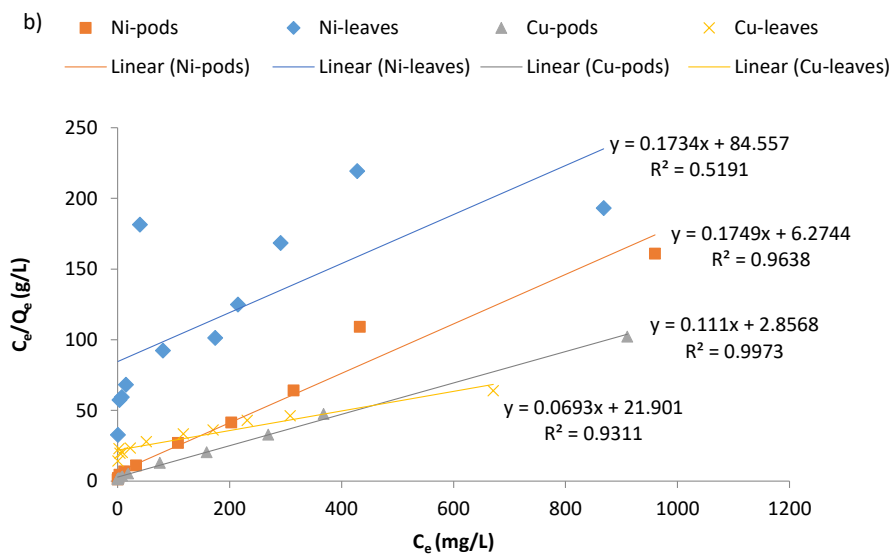
231 The experiment conducted to study the effect of the initial concentration of adsorbate on the  
232 uptake of Ni(II) and Cu(II) ions by *Delonix regia* pods and leaves showed that the uptake of  
233 both metal ions on the two types of adsorbent increased with increasing adsorbate concentration  
234 (Fig. 6a). When adsorbate concentration is increased, there is increased driving force of the



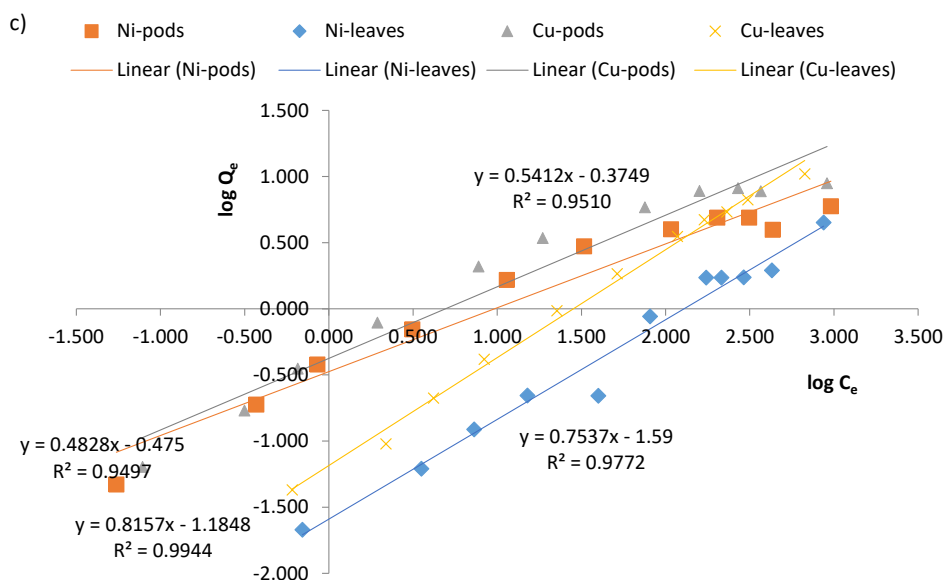
235 metal ions to the binding sites of the adsorbents and thus increase uptake is recorded. Though,  
 236 the uptake per unit gram of adsorbent increased, the opposite which is a decrease was observed  
 237 in the percentage of metal removed from the solution as adsorbate concentration increased.



238



239



240

241 **Figure 6.** Effect of initial metal ions concentration (a), plots of Langmuir (b) and Freundlich  
 242 isotherm (c) isotherms for the adsorption of Ni(II) and Cu(II) ions by *Delonix regia* pods and  
 243 leaves. *Experimental conditions:* pH 4 and 5; contact time: 30 min; metal ions concentration:  
 244 1 - 1000 mg/L  
 245

246 The relatively higher number of metal ions compared to the adsorbent available binding  
 247 surfaces as concentration is increased could be responsible for the decrease observed in  
 248 percentage removal. Thus, it could be said that the uptake of metal ions depends on the initial  
 249 concentration of the adsorbate (Meena et al., 2005).

250 The data obtained from this experiment was modelled using the Langmuir and Freundlich  
 251 isotherm models. Monolayer surface coverage, availability of equal number of adsorption sites  
 252 on the adsorbent and no interaction between adsorbed species were assumptions of the  
 253 Langmuir model (Liu and Wang, 2014). The Langmuir Isotherm is represented in Equation 3

$$254 \quad \frac{C_e}{Q_e} = \frac{1}{Q^0 b} + \frac{C_e}{Q^0} \quad 3$$

255 where  $Q_e$  (mg/g), is the amount of solute adsorbed per unit mass of adsorbent;  $C_e$  (mg/L) is the  
 256 equilibrium concentration of solute in the bulk solution,  $Q^0$  (mg/g) represent the monolayer  
 257 adsorption capacity of the adsorbent and  $b$  (L/mg) represents the constant related to the energy  
 258 of adsorption. The Langmuir equation could be further expressed using a dimensionless



259 constant separation factor  $K_R$  shown in Equation 4.  $K_R$  is a relationship containing all the  
 260 essential features of the Langmuir isotherm.

$$261 \quad K_R = \frac{1}{1 + K_a C_i} \quad 4$$

262 where  $C_i$  is the initial concentration of metal ions in solution (mg/L) and  $K_a$  stands for the  
 263 Langmuir constant (L/mg). This dimensionless separation factor is interpreted to imply that the  
 264 isotherm is favourable if  $0 < K_R < 1$ . The results presented in Fig. 6b for the Langmuir Isotherm  
 265 model showed that for the pods the Langmuir isotherm is favourable for its adsorption of Ni(II)  
 266 and Cu(II) ions. The values obtained for the adsorption of the metal ions onto the leaves showed  
 267 that adsorption of Cu(II) ions onto the leaves is more favourable than that of Ni(II) ions.

268

269 The plot of the Langmuir isotherm also revealed that the curves are continuous leading to  
 270 saturation thus suggesting the possible monolayer coverage of the metal ions on the adsorbent  
 271 surface except for the sorption of Ni(II) ions to the leaves where slight fluctuations were  
 272 noticed. The high correlation coefficient ( $R^2$ ) obtained for the isotherm when  
 273 sorption was carried out using the pods of *Delonix regia* is also an indication of its applicability  
 274 in the sorption reaction. The correlation coefficient obtained using *Delonix regia*  
 275 leaves as adsorbent were not as high as those obtained as the correlation for the pods, implying  
 276 that Langmuir Isotherm is not the best model to explain the sorption of Ni(II) and Cu(II) onto  
 277 the leaves. The parameters obtained for the Langmuir isotherm modelling are shown in Table  
 278 2.

279

280 **Table 2.** Isotherm models adsorption parameters for the adsorption of Ni(II) and Cu(II) onto  
 281 *Delonix regia*

Metal ions	Langmuir Isotherm				Freundlich Isotherm		
	$Q^0$ (mg/g)	b (L/mg)	$R^2$	$K_R$	$K_F$ (mg/g)	1/n	$R^2$
<b>Pods</b>							
Ni	5.88	0.02	0.9638	0.32	0.66	0.34	0.9497
Cu	9.12	0.03	0.9973	0.24	0.86	0.39	0.9510
<b>Leaves</b>							
Ni	5.77	0.0021	0.5191	0.83	0.03	0.75	0.9772
Cu	9.01	0.0389	0.9311	0.21	0.07	0.81	0.9944

282



283 The Freundlich isotherm represented in Equation 5 states that the ratio of the amount of solute  
284 adsorbed onto a given mass of the adsorbent to the concentration of the solute in the solution  
285 is not constant at different concentration. It is an isotherm used to describe adsorption onto  
286 heterogeneous surfaces.

$$287 \quad \log Q_e = \log K_F + \frac{1}{n} \log C_e \quad 5$$

288 where  $1/n$  is the constant related to the adsorption efficiency,  $K_F$  is the adsorption capacity,  $Q_e$   
289 is the quantity of adsorbate adsorbed per unit weight of the adsorbent and  $C_e$  is the final  
290 concentration of metal in the solution. The Freundlich constant  $1/n$  is a factor giving an  
291 indication of how favourable the adsorption of the adsorbate onto the sorbent is,  $0 < 1/n < 1$   
292 imply favourable adsorption. It is also related to the heterogeneity of the adsorbent surface.  
293 The plot of the Freundlich isotherm is presented in Fig. 6c.

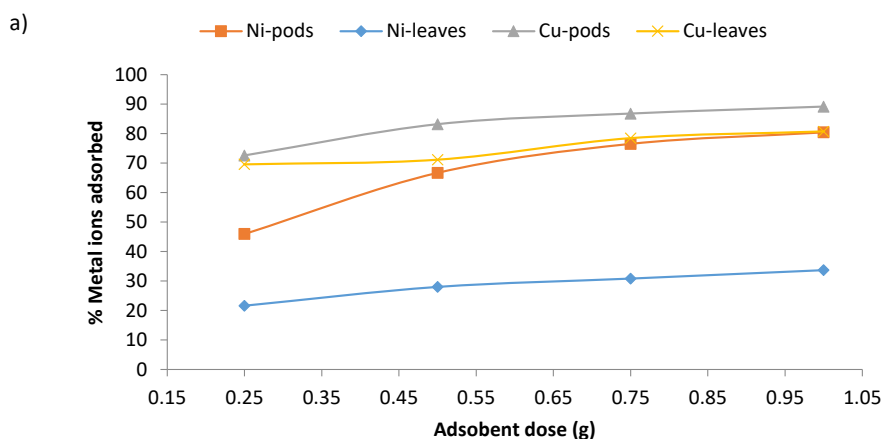
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295 Using the Freundlich isotherm model on the data obtained from the concentration study, it was  
296 discovered from the values of the adsorption parameters shown in Table 2 that the adsorption  
297 of Ni(II) and Cu(II) ions onto *Delonix regia* leaves is more favourable than the adsorption of  
298 these metal ions onto the pods. Values obtained for  $1/n$  are 0.75 and 0.81 for the adsorption of  
299 Ni(II) and Cu(II) ions, respectively for the leaves while the values for their respective sorption  
300 onto the pod are 0.34 and 0.39, respectively. To support this observation, the values obtained  
301 for the correlation coefficient ( $R^2$ ) during the adsorption onto the leaves are higher than those  
302 obtained for the adsorption onto the pods. Thus, the Freundlich isotherm is a better isotherm to  
303 describe the adsorption of Ni(II) and Cu(II) ions onto *Delonix regia* leaves while Langmuir  
304 isotherm is better fitted to describe adsorption onto the pods.

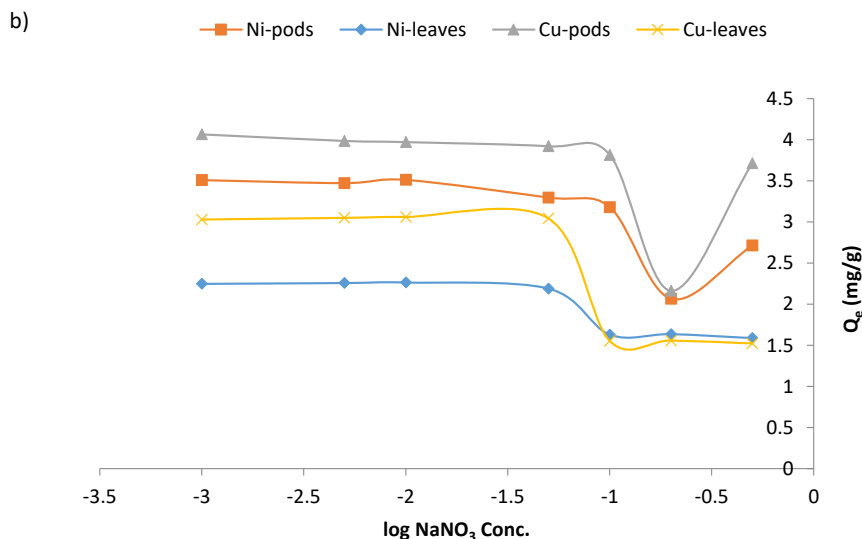
#### 305 3.2.4 Adsorbent dose and solution's ionic strength

306 Fig. 7a revealed the results of the effect of changing the adsorbent doses on the adsorption of  
307 Ni(II) and Cu(II) ions by *Delonix regia* biomass. It was observed that the percentage adsorption  
308 of Ni(II) ions increased from 45.9% to 80.4% and from 21.6% to 33.7% onto the pods and  
309 leaves, respectively, whereas, the percentage adsorption of Cu(II) ions onto both adsorbent  
310 increased from 72.6% to 89.2% and from 69.6% to 80.8% onto the pods and leaves,  
311 respectively. The observed increase in the percentage Ni(II) and Cu(II) ions adsorption might  
312 be due to the availability of more binding sites as adsorbent doses are increased.

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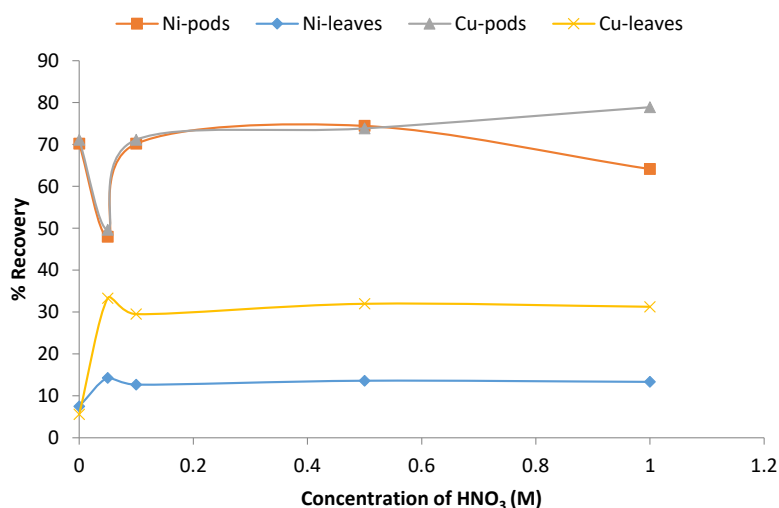
316 **Figure 7.** Effect of adsorbent dose (a) and ionic strength (b) on the adsorption of Ni(II) and  
317 Cu(II) ions by *Delonix regia* pods and leaves. *Experimental conditions:* pH 4 and 5; contact  
318 time: 30min; metal ions concentration: 100 mg/L  
319

320 The result of the effect of sodium ion on the adsorption of Ni(II) and Cu(II) ions by *Delonix*  
321 *regia* biomass is shown in Fig. 7b. The figure showed a reduction in the uptake of both metal  
322 ions by each of the biomass. It could be explained that there was competition for the available  
323 binding sites on the adsorbents by the positive sodium ions present in the adsorption medium.  
324 Thus, as the concentration of sodium ion is increased metal uptake by the adsorbent was  
325 observed to be lower.



326 3.3 Desorption Study

327 The recovery experiment was carried out to investigate the possibility of recovering the  
328 adsorbed metal ions from the biomass. The result obtained from the recovery study is shown  
329 in Fig. 8.



330  
331 **Figure 8.** Recovery study of the adsorbed Ni(II) and Cu(II) ions from the pods and leaves of  
332 *Delonix regia*

333

334 From Fig. 8, the values obtained for the percentage recovery of Ni(II) and Cu(II) ions from the  
335 pods of *Delonix regia* were very similar at different concentration of the desorbing solution,  
336 whereas, when the leaves was considered, different percentages were recovered at different  
337 concentration of the desorbing medium. The figure also revealed that the percentage of metal  
338 ions recovered from the pods were higher than what was recovered from the leaves at various  
339 concentration of nitric acid except at 0.0 M when the percentage obtained were very close to  
340 each other. At this concentration (0.0 M) level, ultra-pure water (milli Q water) was used for  
341 desorbing the metal ions from the adsorbent. Approx. 74.4% Ni(II) ions and 78.9% Cu(II) ions  
342 was recovered from *Delonix regia* pods when the concentration of nitric acid used for  
343 desorbing the metal ions was 0.5 M and 1.0 M, respectively. Moreover, 14.3% Ni(II) ions and  
344 33.3% Cu(II) ions was recovered from the *Delonix regia* leaves with 0.05 M nitric acid. The  
345 recovery experiment showed that metal ions recovery increased with increasing concentration  
346 of nitric acid.





347 **4. Conclusion**

348 The study concerns the application of powdered *Delonix regia* pods and leaves for the removal  
349 of Ni(II) and Cu(II) ions from aqueous solutions. The results obtained indicated that the pH of  
350 the solution, contact time, initial metal ion concentrations, adsorbent dose and ionic strength  
351 affect the uptake of the metal ions by the biosorbent. It was observed that the Freundlich  
352 isotherm is a better isotherm to describe the adsorption of Ni(II) and Cu(II) ions onto *Delonix*  
353 *regia* leaves, while, Langmuir isotherm is better fitted to describe the adsorption onto the pods.  
354 The pseudo-second-order kinetic model agrees with the sorption of Ni(II) and Cu(II) ions onto  
355 *Delonix regia* pods and leaves. The desorption study also showed that the recovery of the metal  
356 ions from the spent pods and leaves increased with increasing concentration of nitric acid.  
357 Thus, powdered *Delonix regia* pods and leaves could be used as an eco-friendly, economically  
358 cheap and effective adsorbents for the removal of Ni(II) ions, Cu(II) ions and other  
359 environmental contaminants from aqueous solution.

360

361 **Data availability**

362 The data generated and/or analysed during the current research are available with the authors  
363 upon reasonable request.

364

365 **Author contributions**

366 BMB was the investigator and contributed to writing the paper. AOB was involved in the  
367 characterization of the adsorbent. COA and OSA were involved in the adsorption studies and  
368 modelling of the adsorption data. SFA and EOO contributed to the writing of the paper.

369

370 **Conflict of Interest**

371 On behalf of the authors, the corresponding author states that there is no conflict of interest.

372

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