

1 **Adsorption and Desorption studies of *Delonix regia* pods and leaves:**  
2 **Removal and recovery of Ni(II) and Cu(II) ions from aqueous solution**

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11 **Abstract**

12 In this study, the adsorption of Ni(II) and Cu(II) ions from aqueous solutions by powdered pods  
13 and leaves of *Delonix regia* was investigated by batch adsorption techniques. The effects of  
14 operating conditions such as pH, contact time, adsorbent dosage, metal ions concentration and  
15 the presence of sodium ions interfering on the sorption process were investigated. The results  
16 obtained showed that the equilibrium sorption was attained within 30 min of interaction, an  
17 increase in the initial concentration of the adsorbate, pH and adsorbent dosage led to increase  
18 in the amount of Ni(II) and Cu(II) ions adsorbed. The adsorption process followed the pseudo-  
19 second-order kinetic model for all the metal ions sorption. The equilibrium data fitted well with  
20 both the Langmuir and Freundlich Isotherms, the monolayer adsorption capacity ( $Q^0$  mg/g) of  
21 the pods and leaves of *Delonix regia* for Ni(II) ions was 5.88 mg/g and 5.77 mg/g, respectively,  
22 and 9.12 mg/g and 9.01 mg/g, respectively for Cu(II) ions. The efficiency of the powdered pods  
23 and leaves of *Delonix regia* for Ni(II) and Cu(II) ions removal was > 80%, except for the  
24 sorption of Ni(II) ions onto the leaves. The desorption study revealed that the percentage of  
25 metal ions recovered from the pods were higher than the leaves at various concentrations of  
26 nitric acid. This study has proven that *Delonix regia* biomass, an agro-waste could be used for  
27 removing Ni(II) and Cu(II) ions from aqueous solution.

28 **Keywords:** *Delonix regia*, low-cost adsorbent, Ni(II) ions, Cu(II) ions, equilibrium, kinetics

## 38 **1. Introduction**

39 The persistent nature, non-biodegradability, toxicity and ability to bio-accumulate in the  
40 environment have made heavy metals priority pollutants (Hamza et al., 2013). Various health  
41 effects are caused by anthropogenic pollutants in water; which are majorly heavy metals such  
42 as mercury, nickel, lead, cadmium copper, zinc and cobalt (Hamza et al., 2013; Singh et al.,  
43 2011). Heavy metals gain entrance into water resources by industrial activities such as  
44 electroplating, smelting, production of glass, textile, paper and ceramics, mining, textiles,  
45 storage batteries, petroleum, metal finishing, pulp and paper (Dean et al., 1972; Ksakas et al.,  
46 2018; Kumar et al., 2019). The damage caused by copper to the marine life include damage of  
47 gills, liver, nervous system, kidneys and changing the sexual life of fishes (Flemming and  
48 Trevors, 1989; Ho et al., 2002; Van Genderen et al., 2005). Although, copper is known to play  
49 a vital role in the metabolism in animal; its excessive intake can result in serious health  
50 problems (Paulino et al., 2006). The permissible limit of copper in wastewater and portable  
51 water is 0.5 mg/L and 2.5 mg/L, respectively (Zhou et al., 2018; Kumar et al., 2019). Reactive  
52 free oxygen species which damage lipids, proteins and DNA are released when copper is  
53 present in the blood system (Brewer, 2010). Wilson's and Alzheimer's diseases, mental illness,  
54 Indian childhood cirrhosis and schizophrenia are also reported to be caused by excess copper  
55 in the blood (Brewer, 2007; Faller, 2009; Hurean and Faller, 2009). Nickel has detrimental  
56 effects on human health, resulting in allergic dermatitis, immunologic urticarial; immediate  
57 and delayed hypersensitivity (Festus et al., 2013). All nickel compounds, except for the metallic  
58 nickel, have been classified as human carcinogens by the International Agency for Research  
59 on Cancer (IARC) (IARC, 1990) and the U.S. Department of Health and Human Services  
60 (DHHS, 1994). Due to its toxicity in minute quantity, 0.05 mg/L was set for the permissible  
61 limit of nickel in wastewater (Zhou et al., 2018).

62 Conventional methods for the removal of metal ions includes: chemical precipitation,  
63 oxidation/reduction, ion exchange, electrochemical processes, membrane separation, Fenton  
64 process, ozonisation, electrocoagulation, photochemical degradation and evaporation (Okoya  
65 et al., 2014). These techniques require high operational costs and yield minimal removal  
66 efficiencies, they have been reported to be expensive and inadequate. Therefore, there is the  
67 need to investigate alternative techniques that are cheaper, efficient and easy to handle. One of  
68 such techniques is biosorption, that is, the use of low-cost adsorbent like agricultural materials  
69 of no economic value and industrial by-products (Jeme, 1968; Inoue and Munemori, 1979) for  
70 the removal of heavy metal ions from polluted water.

71 Almond shells tree bark treated with formaldehyde and sulphuric acid (Guibal et al., 1993; Raji  
72 et al., 1997), bone char, tea leaves, wood charcoal (Ajmal et al. 2003), and coconut shells have  
73 been used to produce activated carbon to remove heavy metal ions from wastewater. Rice hulls  
74 (Ajmal et al., 2003), rice bran (Montanher et al., 2005) and pine bark (Nath et al., 1997) have  
75 also been used in the raw and treated form to remove heavy metal ions. The removal of Ni(II)  
76 ions from aqueous solution using sugarcane bagasse, an agricultural waste biomass, has been  
77 investigated by Garg et al. (2008). The dosage for maximum removal of Ni(II) ions from an  
78 aqueous solution of 50 mg/L were reported to be at 1500 mg/L adsorbent dosage and at pH 7.5.  
79 Moodley et al. (2011) investigated the adsorption capacity of pine sawdust by treating  
80 wastewater containing Ni(II), and other metal ions (Co(II) and Fe(III) ions). The adsorption  
81 and desorption of Ni(II) Ions from aqueous solution by a lignocellulose/montmorillonite  
82 nanocomposite was reported by Zhang and Wang (2015). Their report indicated that the  
83 maximum adsorption capacity of Ni(II) ions reached 94.86 mg/g at an initial Ni(II) ions  
84 concentration of 0.0032 mol/L, a solution pH of 6.8, temperature of 70°C, and contact time of  
85 40 min. Kahraman et al. (2008) examined the use of cotton stalk and apricot seeds as alternative  
86 adsorbents for the removal of Pb and Cu. The removal of Pb and Cu by these agricultural wastes  
87 was reported to reducing their toxic effects on *P. aeruginosa*. The sorption capacity of Cu(II),  
88 kinetics and isotherms of different low-cost residual agricultural materials including peanut  
89 shells, nut shells, plum seeds, eucalyptus bark, olive pips, peach stones, and pine sawdust was  
90 studied by Hansen et al. (2010). Moreover, Abdel-Tawwab et al. (2017) used rice straw,  
91 sugarcane bagasse, and maize stalks for the removal of Pb, Cd, Cu, and Zn from aqueous  
92 solution. All the biosorbents were reported to be effective and cheap for the removal of the  
93 metal ions from polluted water, with rice straw showing a higher adsorption efficiency than the  
94 others. The application of treated pumpkin husk as an excellent adsorbent for removing Cu(II)  
95 and Ni(II) ions has been reported by Samuel et al. (2016). The adsorption of Cu(II) and Ni(II)  
96 ions was found to be suitable at pH 5.

97 *Delonix regia* also known as flame of forest, is a semi-deciduous tree, native to Madagascar. It  
98 is popularly grown in Africa and Hong Kong as a shade tree and for ornamental purpose. The  
99 tree has pods that can be as long as 60 cm in length and 5 cm wide, with a distinct bright green  
100 fern-like compound leaves and attractive red peacock flowers. Researchers have reported the  
101 usefulness of the green leaves and flowers of *Delonix regia* in medicine i.e. *Delonix regia* have  
102 a broad spectrum of pharmacological activities in various ailments (Modi et al., 2016).  
103 However, it sheds its leaves and flowers in dry areas and seasons, the trees are less attractive

104 after the leaves and flowers are shed, with their pods remaining on the branches until they are  
105 dropped by wind, these make *Delonix regia* an agro-waste with limited valuable use.

106 There are limited studies on the use of *Delonix regia* for the removal of organic and inorganic  
107 contaminants from aqueous solution, except for Ponnusami et al. (2009), Onwuka et al. (2016)  
108 and Babalola et al. (2019) who have reported the viability of *Delonix regia* for the removal of  
109 methylene blue dye, crude oil spill and Pb(II) ions, respectively. Therefore, the objective of  
110 this research is to investigate the capacity of the pods and leaves of *Delonix regia* in the removal  
111 of Ni(II) and Cu(II) ions from aqueous solutions. The desorption of bound metals from spent  
112 *Delonix regia* pods and leaves using various concentrations of nitric acid was also considered.

## 113 **2. Materials and methods**

### 114 2.1 *Delonix regia* sample

115 Leaves and pods of *Delonix regia* collected from Ekiti State University, Ado-Ekiti, Nigeria  
116 were used as adsorbent for the sorption study. The materials were washed with deionised water,  
117 sun-dried and milled. After milling, the adsorbents were sieved through a 250 $\mu$ m mesh nylon  
118 sieve and kept in air tight containers until required for use.

### 119 2.2 Chemicals and reagents

120 Diammonium nickel hexahydrate and copper chloride dihydrate salts supplied by Merck,  
121 Germany were dissolved in high purity milli-Q water to prepare 1000 mg/L stock solutions of  
122 Ni(II) and Cu(II) ions, respectively. Working standard solutions were prepared from the stock  
123 solutions and pH adjustment was done with 0.1 M HNO<sub>3</sub> and 0.1 M NaOH when necessary.  
124 The effect of solution ionic strength on sorption was studied using different concentrations of  
125 sodium nitrate salt and desorption of bound metal from spent biomass was achieved with  
126 different concentrations of HNO<sub>3</sub>.

### 127 2.3 Characterization

128 The elemental composition of the pods and leaves of *Delonix regia* was achieved by energy  
129 dispersive spectroscopy (EDS). The morphological study was by the scanning electron  
130 microscope (Nova Nano SEM 230) and the transmission electron microscope (FEI Tecnai G<sup>2</sup>  
131 20). X-ray diffractometer (Siemens D8 Advance Bruker XRD) was used for the phase  
132 characterization.

133

134

## 135 2.4 Adsorption

136 Adsorption procedure by Meena et al. (2008) was slightly modified and used in this work.  
137 Parameters such as the influence of pH, contact time, initial adsorbate concentration, adsorbent  
138 dosage and solution's ionic strength were investigated.

139 For the influence of pH, a 0.5 g of the biomass was weighed into designated tubes containing  
140 20 mL of 100 mg/L metal ions solution of various pH in the range 1 to 8. The suspensions were  
141 shaken on an end-over-end shaker for 300 min at ambient temperature ( $21\pm 2^\circ\text{C}$ ). The influence  
142 of contact time was conducted by varying the contact time from 5 - 300 min at optimised pH.  
143 The concentration of Ni(II) and Cu(II) ions was varied from 1 - 1000 mg/L for the influence  
144 of initial metal ions concentration at optimised pH and contact time. Finally, the influence of  
145 adsorbent dosage and solution's ionic strength was achieved using 100 mg/L metal ions  
146 concentration, the parameters were varied from 0.25 - 1.0 g and 0.001 - 0.5 M  $\text{NaNO}_3$ ,  
147 respectively at optimised pH and contact time. Each of the experiment was carried out in  
148 triplicate and the results were the average values.

149 At the expiration of each of the experiment, aliquot was taken, centrifuged (twice at 4500 rpm  
150 for 15 min and 10300 rpm for 10 min) and diluted with 0.1 M  $\text{HNO}_3$  before the residual metal  
151 content was analysed by Thermo elemental inductively coupled plasma – mass spectroscopy  
152 (ICP-MS; X Series II).

## 153 2.5 Analytical procedure

154 Multi-elements standard solution was used to prepare different concentrations of external  
155 calibration standard solutions (1 – 100  $\mu\text{g/L}$ ) used for the analysis. After the instrument was  
156 switched to the operate mode, the pressure of the nebulizer was checked, and the instrument's  
157 sensitivity and stability were checked by running a tuning solution of 1  $\mu\text{g/L}$  multi element  
158 standard solution for 10 min. It was ensured that the  $^{115}\text{In}$  counts was less than 20 K counts per  
159 second, precision less than 2%. The backgrounds (5BKg and 220BKg) were less than 1 count  
160 per second, the oxides cerium oxide ( $\text{CeO}^+$ ) less than 2.0% and the doubly charged ions ( $\text{Ba}^{2+}$ )  
161 less than 6.0%. Therefore, the calibration standard solution and the blank were analysed to  
162 obtain a calibration curve where the samples to be analysed will properly fit. The analysis of  
163 the samples proceeded after the calibration curve for each of the metal ions was good with  $R^2$   
164 = 0.9999.

165 The amount of Ni(II) and Cu(II) ions sorbed on the pods and leaves of *Delonix regia* ( $Q_e$ ) was  
166 calculated using Equation 1.

167  $Q_e = (C_o - C_e)V/m$  1

168 where  $C_o$  is the initial metal concentration (mg/L),  $C_e$  is the final metal ion concentration in the  
 169 solution, ICP-MS reading (mg/L),  $V$  is the volume of the metal solution used in litre (L) and  
 170  $m$  is the mass of the biosorbent (g).

171 2.6 Kinetics and Equilibrium modelling

172 Further examination of the contact time experiment was carried out by modelling the data with  
 173 the pseudo-second-order kinetic models to determine the mechanism of the sorption process.

174 The pseudo-second-order kinetic model can be expressed in Equation 2 where  $k_2$  (g/mg/min)  
 175 represent the rate constant for the pseudo-second-order kinetics;  $Q_e$  and  $Q_t$  (both in mg/g) being  
 176 the amount of adsorbate taken up by the adsorbent at equilibrium and at time  $t$ , respectively.  
 177 All parameters in Equation 2 were derived by plotting  $t/Q_t$  against  $t$ .

178  $t/Q_t = 1/k_2 + t/Q_e$  2

179 The data obtained on the effect of initial metal ions concentration was also modelled using the  
 180 Langmuir and Freundlich isotherms. Monolayer surface coverage, availability of equal number  
 181 of adsorption sites on the adsorbent and no interaction between adsorbed species were  
 182 assumptions of the Langmuir model (Liu and Wang, 2014). The Langmuir Isotherm is  
 183 represented in Equation 3

184  $\frac{C_e}{Q_e} = \frac{1}{Q^0 b} + \frac{C_e}{Q^0}$  3

185 where  $Q_e$  (mg/g), is the amount of solute adsorbed per unit mass of adsorbent;  $C_e$  (mg/L) is the  
 186 equilibrium concentration of solute in the bulk solution,  $Q^0$  (mg/g) represent the monolayer  
 187 adsorption capacity of the adsorbent and  $b$  (L/mg) represents the constant related to the energy  
 188 of adsorption. The Langmuir equation could be further expressed using a dimensionless  
 189 constant separation factor  $K_R$  shown in Equation 4.  $K_R$  is a relationship containing all the  
 190 essential features of the Langmuir isotherm.

191  $K_R = \frac{1}{1 + K_a C_i}$  4

192 where  $C_i$  is the initial concentration of metal ions in solution (mg/L) and  $K_a$  stands for the  
 193 Langmuir constant (L/mg). This dimensionless separation factor is interpreted to imply that  
 194 the isotherm is favourable if  $0 < K_R < 1$ .

195 The Freundlich isotherm states that the ratio of the amount of solute adsorbed onto a given  
196 mass of the adsorbent to the concentration of the solute in the solution is not constant at  
197 different concentration. The Freundlich isotherm is used to describe adsorption onto  
198 heterogeneous surfaces (Equation 5).

$$199 \log Q_e = \log K_F + \frac{1}{n} \log C_e \quad 5$$

200 where  $1/n$  is the constant related to the adsorption efficiency,  $K_F$  is the adsorption capacity,  $Q_e$   
201 is the quantity of adsorbate adsorbed per unit weight of the adsorbent and  $C_e$  is the final  
202 concentration of metal in the solution. The Freundlich constant  $1/n$  is a factor giving an  
203 indication of how favourable the adsorption of the adsorbate onto the sorbent is,  $0 < 1/n < 1$   
204 imply favourable adsorption. It is also related to the heterogeneity of the adsorbent surface.

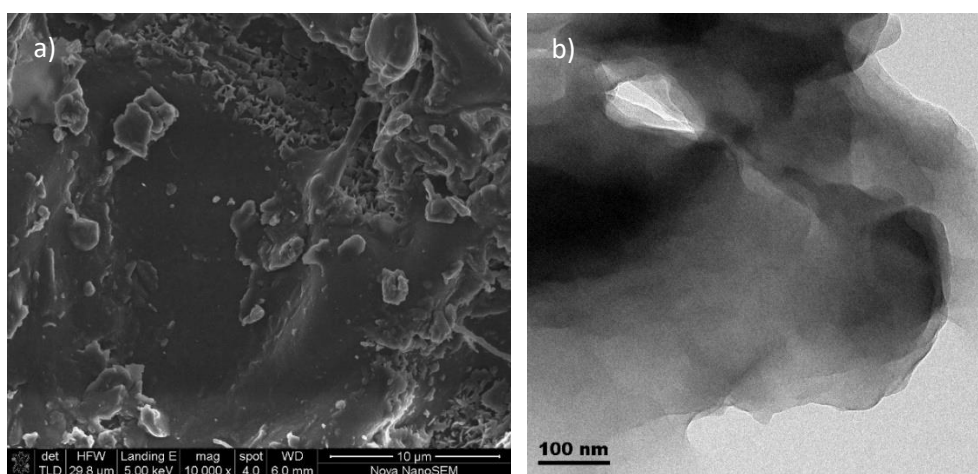
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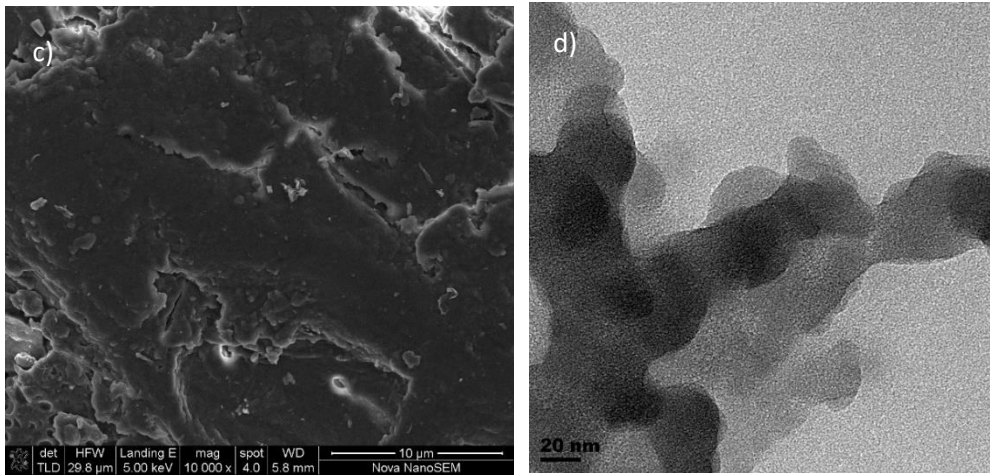
### 206 3. Results and discussion

#### 207 3.1 SEM-EDS, TEM and XRD analyses

208 The SEM (at x10 000 magnification) and TEM micrographs of the pods and leaves of *Delonix*  
209 *regia* (Fig. 1) indicated the spongy nature of *Delonix regia* with porous structures, being  
210 potentially beneficial for the uptake of the Ni(II) and Cu(II) ions from aqueous solution. The  
211 EDS of *Delonix regia* showed that the surfaces of the leaves was composed of 66.79% C,  
212 32.97% O and traces of Ca and K, while, the pods was composed of 57.61% C, 41.15% O and  
213 trace of K.

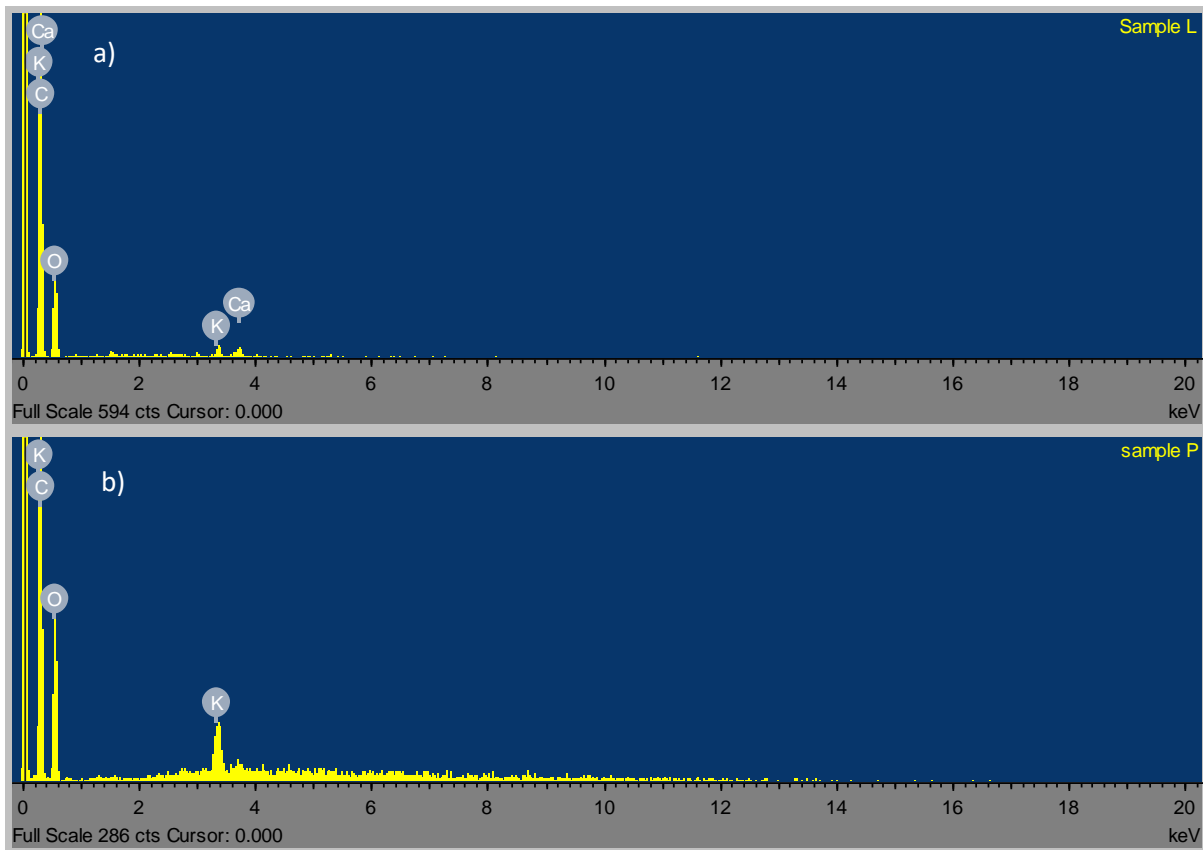
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216  
 217 **Figure 1.** SEM (at x10 000 magnification) and TEM micrographs of *Delonix regia* leaves (a  
 218 & b) and pods (c & d)

219



220

221

222 **Figure 2.** EDS of leaves (a) and pods (b) of *Delonix regia*

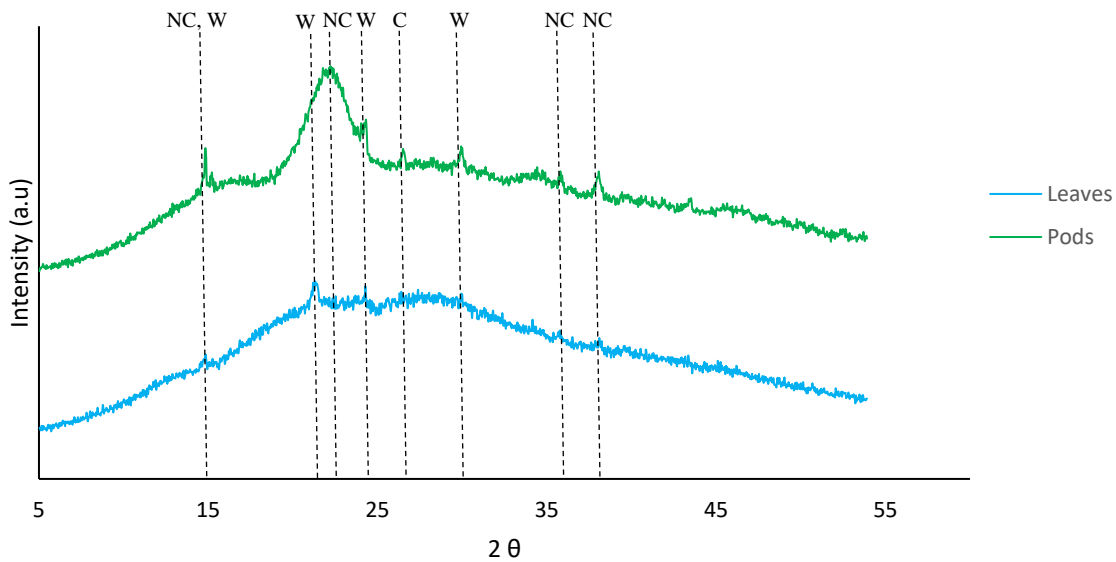
223 According to the ICSD Nos. 03-0289, 20-0231 and 26-1077, native cellulose ( $C_6H_{12}O_6$ )<sub>x</sub> and  
 224 whewellite, syn ( $C_2CaO_4 \cdot H_2O / CaC_2O_4 \cdot H_2O$ ) were identified as major peaks in *Delonix regia*  
 225 (Fig. 3). The pods were mainly native cellulose, whereas, the leaves were rich in whewellite,



226 syn. The hemicellulosic moieties in the pods and leaves might provide sites for the binding of  
227 Ni(II) and Cu(II) ions.

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230

231 **Figure 3.** X-ray diffractogram of the leaves and pods of *Delonix regia*

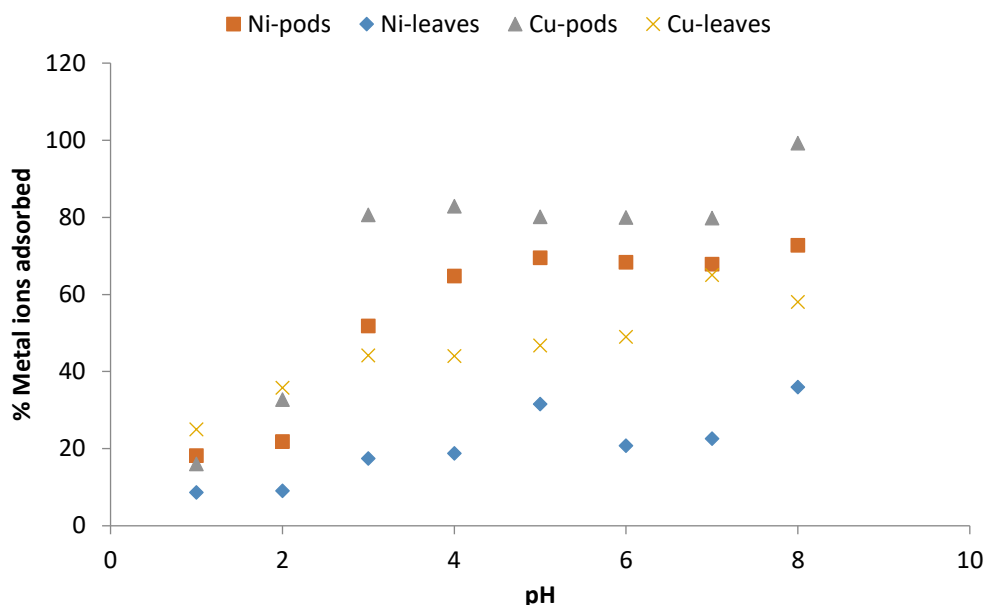
232 (NC – native cellulose ((C<sub>6</sub>H<sub>12</sub>O<sub>6</sub>)<sub>x</sub>); W – whewellite, syn (C<sub>2</sub>CaO<sub>4</sub>·H<sub>2</sub>O/CaC<sub>2</sub>O<sub>4</sub>·H<sub>2</sub>O); C – carbon)

233

### 234 3.2 Adsorption studies

#### 235 3.2.1 pH

236 The result of the study of pH on the adsorption of Ni(II) and Cu(II) ions onto *Delonix regia* is  
237 shown in Fig. 4. The figure reveals that there was no evident nickel uptake by both adsorbents  
238 at low pH, but a very noticeable uptake was achieved as pH increased. pH 5 at which maximum  
239 sorption was recorded was used in subsequent experiments. Saeed et al. (2005b) reported an  
240 optimum sorption pH of 6 for Ni(II) on crop milling waste while pH 5 was reported for its  
241 sorption onto natural neem sawdust and almond husk (Hasar, 2003; Rao et al., 2007), thus  
242 being in line with our findings.



243 **Figure 4.** Effect of pH on the adsorption of Ni(II) and Cu(II) by *Delonix regia* pods and leaves.  
 244 *Experimental conditions:* pH 1-8; contact time: 300 min; adsorbent dosage: 0.5; metal ions  
 245 concentration: 100 mg/L  
 246

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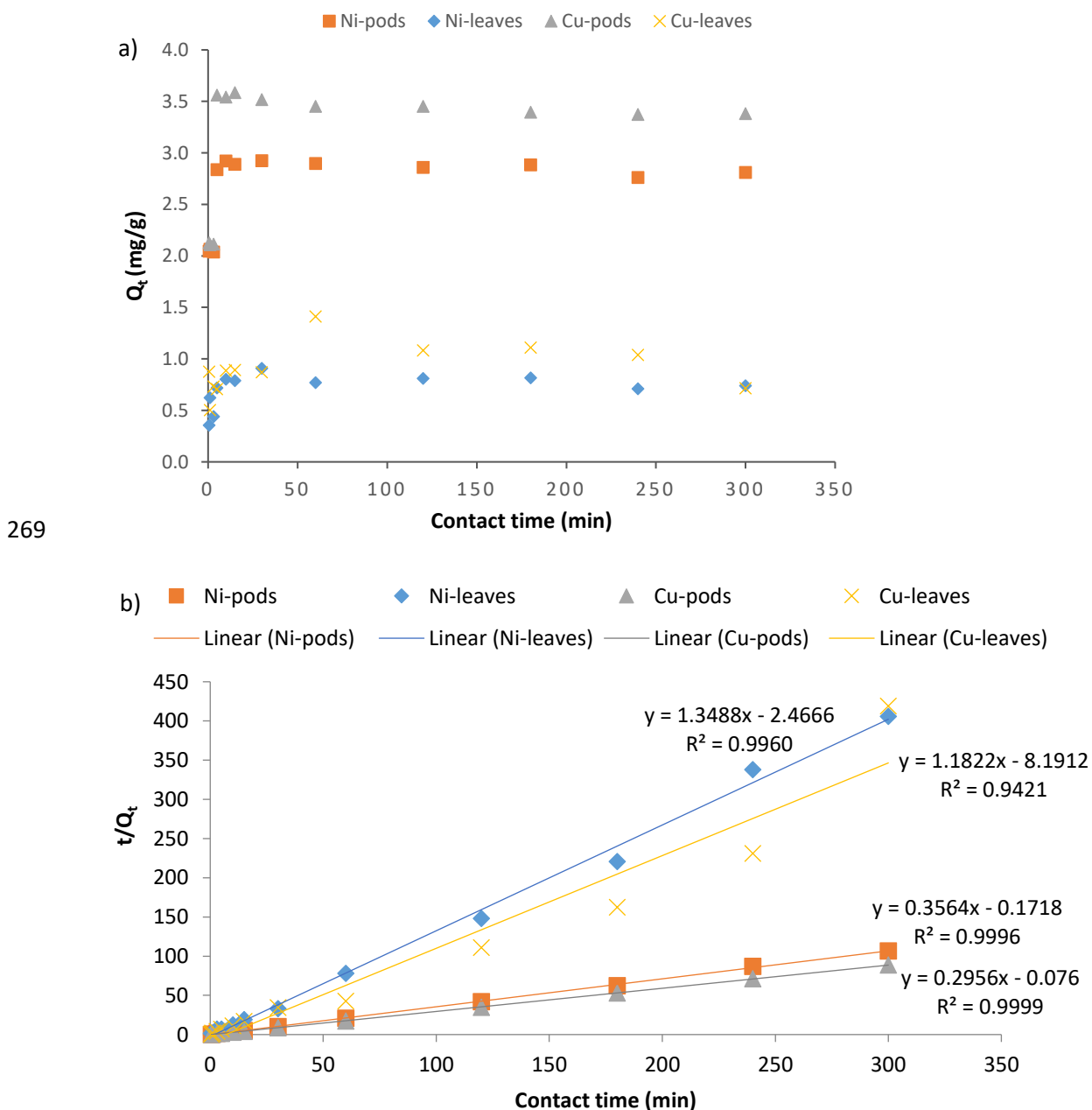
248 A small increase in the uptake value was achieved between pH 1 to 3, but maximum uptake of  
 249 46.7% was recorded at pH 5 for Cu(II) ions sorption onto leaves and maximum uptake of 82.9%  
 250 at pH 4 onto the pods which were further used for adsorption of Cu(II) onto the leaves and  
 251 pods, respectively. The increase recorded at pH 6 and 7 were not considered in choosing the  
 252 optimum pH at which Cu(II) ions sorption onto the leaves occurred because visible precipitate  
 253 which might be due to the formation of  $\text{Cu}(\text{OH})_2$  or other soluble complexes had been formed  
 254 in the experimental set up at these pH (Larous and Meniai, 2012). Some authors reported pH 5  
 255 and 5.8 as the optimum for the uptake of Cu(II) ions by some modified natural wastes (Shukla  
 256 and Pai, 2005; Witek-Krowiak et al., 2011; Anantha and Kota, 2016). This might be as a result  
 257 of the increased overall negative charge particularly between pH 4 and 6 which would  
 258 subsequently lead to increase the sorption of the positive metal ions. The increase of pH  
 259 decreases the concentration of hydrogen ions and therefore the competition between metal ions  
 260 and hydrogen ions for active sites on the adsorbent is reduced (Kadirvelu et al., 2000; Kadirvelu  
 261 et al., 2001; Sánchez-Polo and Rivera-Utrilla, 2002; Kadirvelu et al., 2003; Meena et al.,  
 262 2005a).

263

264

265 3.2.2 Contact time

266 The investigation of the effect of agitation time performed at different time intervals of 5 min  
 267 up to 300 min showed that the two adsorbents used in this work had rapid uptake of the metal  
 268 ions within short period of interaction (Fig. 5a).



270 **Figure 5.** Effect of contact time (a) and pseudo-second-order kinetics (b) of the adsorption of  
 271 Ni(II) and Cu(II) ions by *Delonix regia* pods and leaves. *Experimental conditions:* pH 4 and 5;  
 272 contact time: 5-300 min; adsorbent dosage: 0.5 g; metal ions concentration: 100 mg/L  
 273  
 274

275 A slight desorption and adsorption was observed between 5 to 10 min of interaction of the  
 276 adsorbent with the metal ions solution. Within 30 min of interaction, maximum uptake has

277 been achieved on both adsorbents irrespective of the metal ions considered, though the uptake  
 278 recorded on the pods were higher than those on the leaves. The native cellulose, a major  
 279 component of the pods might be responsible for the enhanced uptake on the pods. Metal uptake  
 280 by the adsorbents remained fairly constant after 30 min of interaction until the end of the  
 281 experiment. Moreover, the maximum uptake at 30 min could be considered to be faster when  
 282 compared with other biosorbents reported in the literature. Olufemi and Eniodunmo (2017)  
 283 reported 30 min and 120 min as the optimum time for the removal of Ni(II) ions from aqueous  
 284 solutions using coconut shell and banana peels, respectively. Ksakas et al. (2018) reported 60  
 285 min and 180 min as the optimum contact time for the sorption of Cu(II) ions unto some types  
 286 of natural clay. Alatabe (2018) reported 120 min as the optimum sorption time for Cu(II) ions  
 287 onto activated carbon from *Cane papyrus*. However, 30 min was the optimum contact time  
 288 reported by Kumar et al. (2019) on the removal of Cu(II) ions by groundnut seed cake powder,  
 289 sesame seed cake powder and coconut cake powder.

290 The kinetic modelling of data showed that the process was well fitted to the pseudo-second-  
 291 order kinetic model. This is supported by Hansen et al. (2010) who reported that the adsorption  
 292 of Cu(II) ions onto various agriculture waste materials fitted the pseudo-second-order kinetic  
 293 model, the plots and kinetic parameters of this model are shown in Fig. 5b and Table 1,  
 294 respectively. The pseudo-second-order kinetic model indicates that the mechanism involved in  
 295 the sorption is governed by ion exchange or sharing of electrons (Babalola et al., 2019).

296

297 **Table 1.** Parameters obtained from the pseudo-second-order kinetic model

Metal ions	Q <sub>e</sub> (mg/g)	k <sub>2</sub> (g.mg <sup>-1</sup> min <sup>-1</sup> )	R <sup>2</sup>
<i>Delonix regia</i> pods			
Ni	2.8	-2.36	0.9996
Cu	3.4	-3.24	0.9999
<i>Delonix regia</i> leaves			
Ni	0.7	-0.25	0.9960
Cu	0.8	-0.09	0.9421

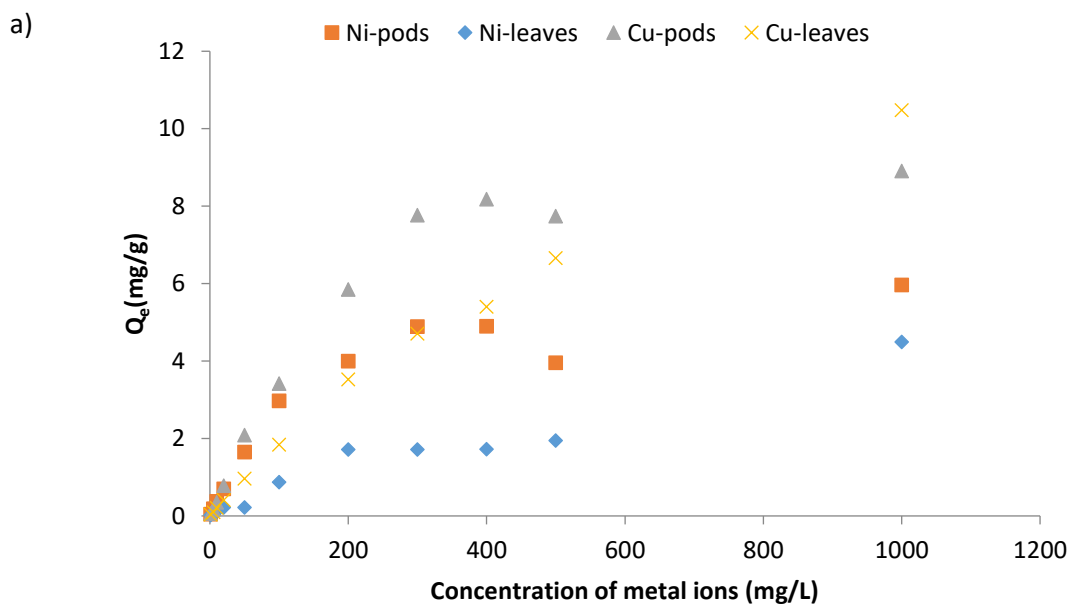
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299 In a similar study by Babalola et al. (2019), the calculated Q<sub>e</sub> value from the pseudo-second-  
 300 order kinetic model of the adsorption of Pb(II) ions onto *Delonix regia* pods and leaves are  
 301 4.12 mg/g and 2.7g mg/g, respectively. Bansal et al. (2009) reported 2.81 mg/g for the sorption  
 302 of Ni(II) ions onto rice husks.

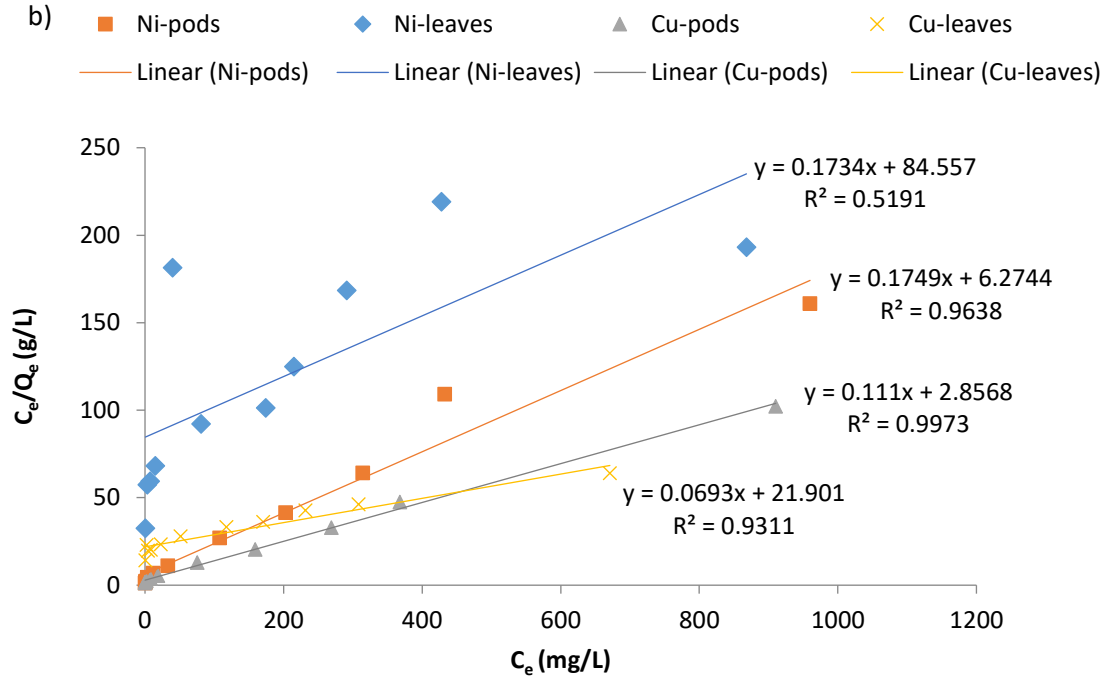
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304 3.2.3 Initial adsorbate concentration and isotherm experiment

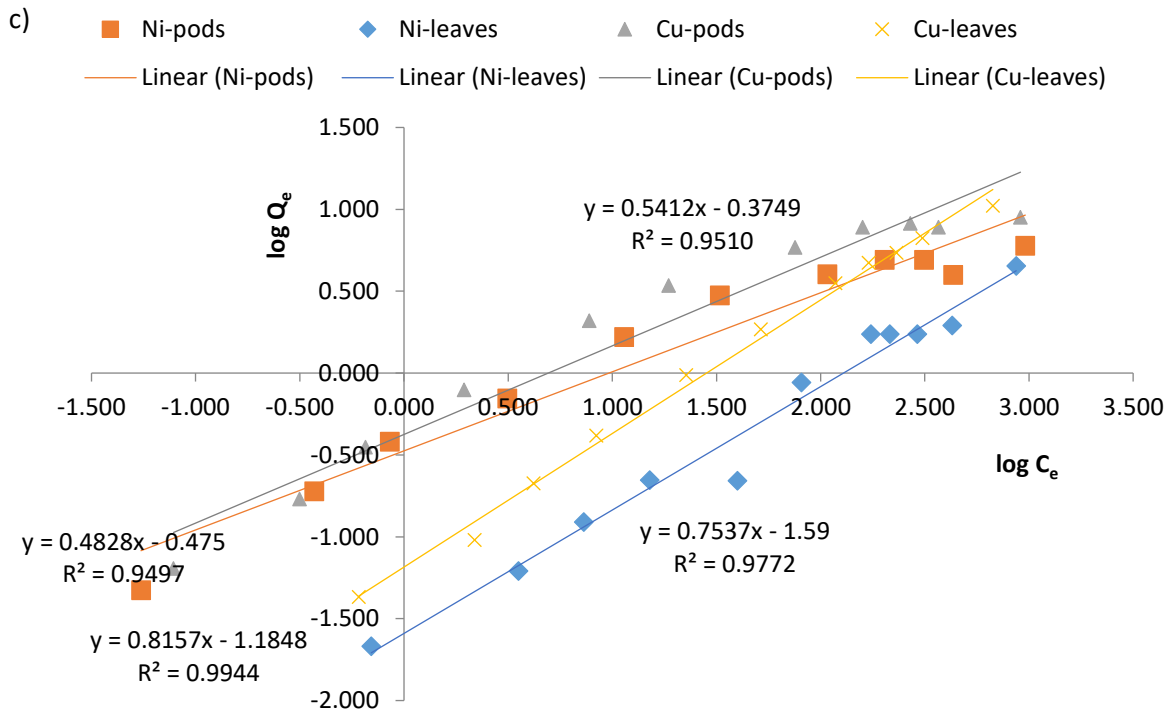
305 The experiment conducted to study the effect of the initial concentration of adsorbate on the  
306 uptake of Ni(II) and Cu(II) ions by the pods and leaves of *Delonix regia* showed that the uptake  
307 of both metal ions on the two types of adsorbent increased with increasing adsorbate  
308 concentration (Fig. 6a). When adsorbate concentration is increased, there is increased driving  
309 force of the metal ions to the binding sites of the adsorbents and thus increased uptake is  
310 recorded. Though, the uptake per unit gram of the adsorbent increased, the opposite which is a  
311 decrease was observed in the percentage of metal removed from the solution as the adsorbate  
312 concentration increased. This is because as the ratio of the metal ions to the adsorbent increases,  
313 the exchangeable sites in the adsorbent structure are saturated, resulting in a decrease in the  
314 percentage removed (Man et al., 2012). The data obtained in Figs. 5a and 6a also suggested  
315 that the pods are better than the leaves and the adsorption is more favourable onto the pods at  
316 all concentrations used in this study.



317



318



319

320 **Figure 6.** Effect of initial metal ions concentration (a), plots of Langmuir (b) and Freundlich  
 321 isotherm (c) isotherms for the adsorption of Ni(II) and Cu(II) ions by *Delonix regia* pods and  
 322 leaves. *Experimental conditions:* pH 4 and 5; contact time: 30 min; adsorbent dosage: 0.5 g;  
 323 metal ions concentration: 1 - 1000 mg/L

324

325 The relatively high concentration of metal ions compared to the adsorbent available binding  
 326 surfaces as concentration is increased could be responsible for the decrease observed in  
 327 percentage removal (Meena et al., 2005b; Hamza et al., 2013). The data obtained from this  
 328 experiment was modelled using the Langmuir and Freundlich isotherm models.

329 The results presented in Fig. 6b for the Langmuir Isotherm model showed that for the pods the  
 330 Langmuir isotherm is favourable for its adsorption of Ni(II) and Cu(II) ions. The values  
 331 obtained for the adsorption of the metal ions onto the leaves showed that adsorption of Cu(II)  
 332 ions onto the leaves is more favourable than that of Ni(II) ions. The fit to the plot of the  
 333 Langmuir isotherm suggests the possible monolayer coverage of the metal ions on the  
 334 adsorbent surface except for the sorption of Ni(II) ions to the leaves where fluctuations were  
 335 observed. The high correlation coefficient ( $R^2$ ) obtained for the isotherm when sorption was  
 336 carried out using the pods of *Delonix regia* is also an indication of its applicability in the  
 337 sorption reaction. The correlation coefficient obtained using *Delonix regia* leaves as adsorbent  
 338 were not as high as those obtained as the correlation for the pods, implying that Langmuir  
 339 Isotherm is not the best model to explain the sorption of Ni(II) and Cu(II) onto the leaves. The  
 340 parameters obtained for the Langmuir isotherm modelling are shown in Table 2.

341

342 **Table 2.** Isotherm models adsorption parameters for the adsorption of Ni(II) and Cu(II) onto  
 343 *Delonix regia*

Metal ions	Langmuir Isotherm				Freundlich Isotherm		
	$Q^0$ (mg/g)	b (L/mg)	$R^2$	$K_R$	$K_F$ (mg/g)	1/n	$R^2$
<b>Pods</b>							
Ni	5.88	0.02	0.9638	0.32	0.66	0.34	0.9497
Cu	9.12	0.03	0.9973	0.24	0.86	0.39	0.9510
<b>Leaves</b>							
Ni	5.77	0.0021	0.5191	0.83	0.03	0.75	0.9772
Cu	9.01	0.0389	0.9311	0.21	0.07	0.81	0.9944

344

345 The plot of the Freundlich isotherm is presented in Fig. 6c. Using the Freundlich isotherm  
 346 model on the data obtained from the concentration study, it was further discovered from the  
 347 values of the adsorption parameters shown in Table 2 that the adsorption of Ni(II) and Cu(II)  
 348 ions onto *Delonix regia* leaves is more favourable than the adsorption of these metal ions onto  
 349 the pods. Values obtained for 1/n are 0.75 and 0.81 for the adsorption of Ni(II) and Cu(II) ions,  
 350 respectively for the leaves while the values for their respective sorption onto the pod are 0.34

351 and 0.39, respectively. The values of the Freundlich constant  $1/n$  which are lower for the pods  
352 and a higher adsorption capacity,  $K_F$  for the pods are further confirmation that the pods adsorb  
353 better than the leaves.

354 The values obtained for the Freundlich isotherm correlation coefficient ( $R^2$ ) during the  
355 adsorption of Ni(II) and Cu(II) ions onto the leaves are higher than those obtained for the  
356 adsorption onto the pods. Thus, the Freundlich isotherm is a better isotherm to describe the  
357 adsorption of Ni(II) and Cu(II) ions onto *Delonix regia* leaves, while, the Langmuir isotherm  
358 is better fitted to describe adsorption onto the pods.

359 Kumar et al. (2019) reported that the sorption of Cu(II) ions onto groundnut seed cake, sesame  
360 seed cake and coconut cake powders fit perfectly to the Langmuir isotherm with  $Q^0$  ranging  
361 from 3.608 to 3.703 mg/g. Likewise, Saeed et al. (2005a) reported the biosorption of Cu(II)  
362 ions to perfectly fit the Langmuir adsorption isotherm model. Olufemi and Eniolaodunmo  
363 (2018) reported a  $Q^0$  of 1.47 mg/g and 2.57 mg/g for the sorption of Ni(II) ions onto banana  
364 peels and coconut shells, respectively, with Langmuir constant  $b$  (L/mg) as 0.018 and 0.016,  
365 respectively. Malkoc and Nuhoglu (2005) recorded a  $Q^0$  of 15.26 mg/g and  $b$  value of 0.088  
366 L/mg for the adsorption of Ni(II) ions onto tea factory waste. Thus, the isotherm experiment  
367 has shown that the Langmuir constant related to the sorption energy obtained in this study were  
368 very close to banana peels, coconut shells and tea waste, except for the adsorption of Ni(II)  
369 ions onto the leaves which was lower. Moreover, the  $Q^0$  of the pods and leaves of *Delonix regia*  
370 in this work were higher than that of banana peels and coconut shells, but lower than what was  
371 obtained for the tea factory waste.

372 In a similar study by Babalola et al. (2019), the Langmuir isotherm provided the best fit for the  
373 adsorption of Pb(II) ions onto the pods of *Delonix regia*, whereas, the Freundlich isotherm also  
374 gave a better fit for the leaves. This implies that the sorption of these metal ions onto the pods  
375 assumes a monolayer adsorption onto a homogeneous surface with a finite number of identical  
376 sites, whereas, sorption onto the leaves assumes that the metal ions adsorb onto the  
377 heterogeneous surface of the adsorbent (Ayanda et al., 2013).

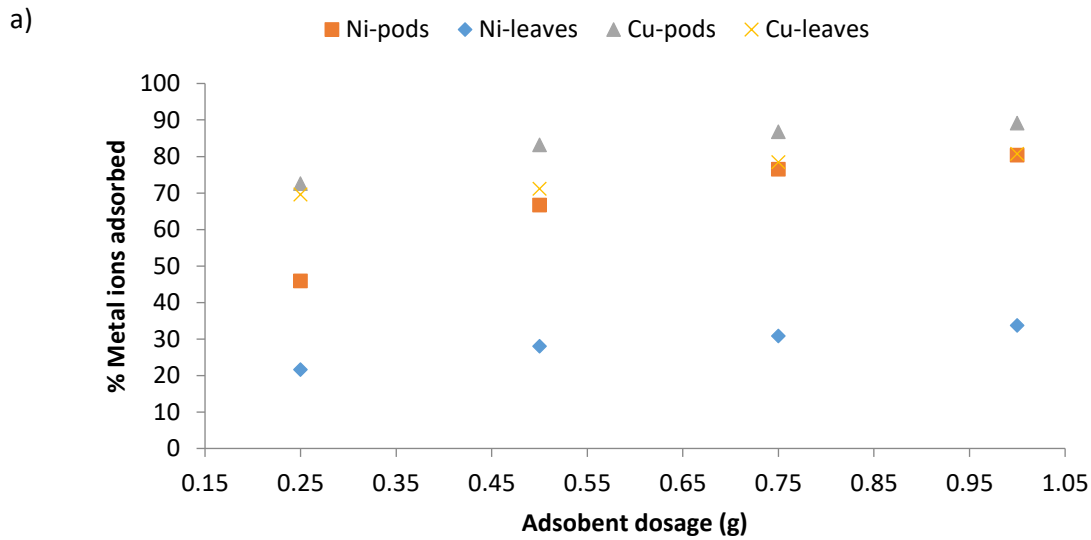
#### 378 3.2.4 Adsorbent dosage and solution's ionic strength

379 Fig. 7a revealed the results of the effect of changing the adsorbent doses on the adsorption of  
380 Ni(II) and Cu(II) ions by *Delonix regia* biomass. It was observed that the percentage adsorption  
381 of Ni(II) ions increased from 45.9% to 80.4% and from 21.6% to 33.7% onto the pods and  
382 leaves, respectively, whereas, the percentage adsorption of Cu(II) ions onto both adsorbent

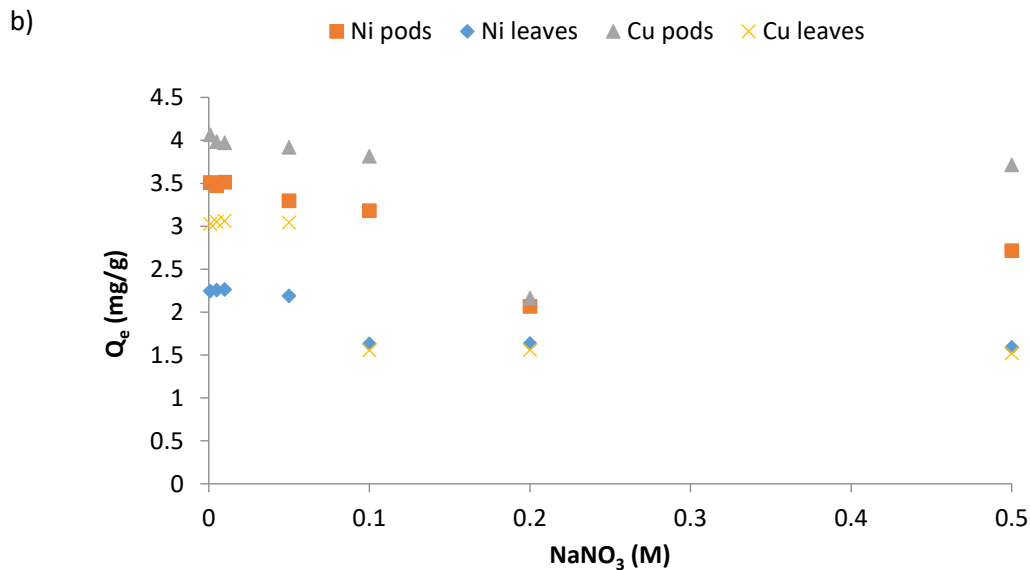


383 increased from 72.6% to 89.2% and from 69.6% to 80.8% onto the pods and leaves,  
 384 respectively. The observed increase in the percentage Ni(II) and Cu(II) ions adsorption might  
 385 be due to the availability of more binding sites as adsorbent doses are increased.

386



387  
388



389

390 **Figure 7.** Effect of adsorbent dosage (a) and ionic strength (b) on the adsorption of Ni(II) and  
 391 Cu(II) ions by *Delonix regia* pods and leaves. *Experimental conditions:* pH 4 and 5; contact  
 392 time: 30min; metal ions concentration: 100 mg/L

393

394 The result of the effect of sodium ion on the adsorption of Ni(II) and Cu(II) ions by *Delonix*  
 395 *regia* biomass is shown in Fig. 7b. The figure shows a reduction in the uptake of both metal

396 ions by each of the biomasses. It could be explained that there was competition for the available  
 397 binding sites on the adsorbents by the positive sodium ions present in the adsorption medium  
 398 (Alegbe et al., 2019). Thus, as the concentration of sodium ion is increased metal uptake by the  
 399 adsorbent was observed to be lower.

400 A comparison of the adsorption efficiency of different agricultural waste for Ni(II) and Cu(II)  
 401 ions is presented in Table 3.

402

403 **Table 3.** Comparison of the amount of Ni(II) and Cu(II) ions removed by some agro-waste  
 404 with the pods and leaves of *Delonix regia*

Agricultural waste	Metal ions	Adsorbent dosage	Efficiency	References
Tea waste	100 mg/L Ni(II)	10 g/L	86%	Malkoc and Nuhoglu, 2005
Saw dust	10 mg/L Ni(II)	5 g/100 ml	75%	Shukla et al., 2005
Sugarcane bagasse	50mg/L Ni(II)	1500 mg/L	> 80%	Garg et al., 2008
Banana peel	100 mg/L Ni(II)	4.5 g/50 mL	78%	Olufemi and Eniolaodunmo 2018
Coconut shell	100 mg/L Ni(II)	4.5 g/50 mL	75%	
Papaya wood	10 mg/L Cu(II)	5 g/L	95%	Saeed et al., 2005a
Rice bran	Cu(II)	200 mg/20 mL	>80%	Montanher et al., 2005
Groundnut seed cake				
Sesame seed cake	10 mg/L Cu(II)	0.75-1 g/50 mL	99.7%	Kumar et al., 2019
Coconut cake				
Spruce Sawdust	10 mg/L Cu(II)	1 g/100 mL	>85%	Kovacova et al., 2019.
<i>Delonix regia</i> pods	100 mg/L Ni(II)		>80%	
<i>Delonix regia</i> leaves	100 mg/L Ni(II)	0.5 g/20 mL	>30%	This study
<i>Delonix regia</i> pods	100 mg/L Cu(II)		>85%	
<i>Delonix regia</i> leaves	100 mg/L Cu(II)		>80%	

405

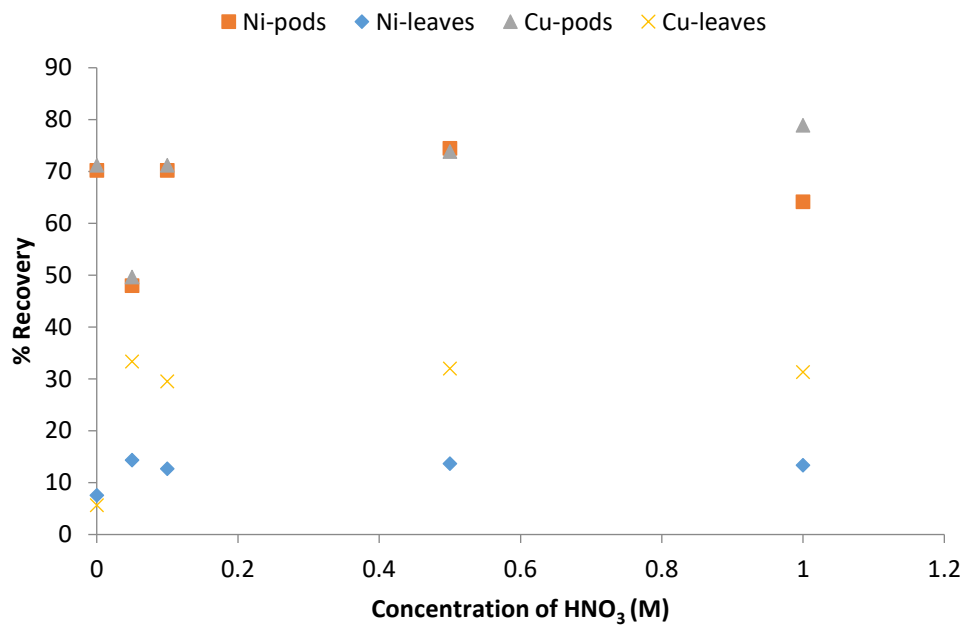
406 The results obtained from this study have shown that *Delonix regia* biomass compete  
 407 favourably with other agricultural waste used in previous studies and hence, could be useful in  
 408 removing Ni(II) and Cu(II) ions from aqueous solution.

409

### 410 3.3 Desorption Study

411 The regeneration of adsorbents after adsorption is of outmost importance, metal ions adsorbed  
 412 should be easily desorbed under suitable conditions and the adsorbents should be repeatedly  
 413 use to reduce the cost of the material. Thus, the recovery experiment was carried out to

414 investigate the possibility of recovering the adsorbed metal ions from the biomasses. The result  
415 obtained from the recovery study is shown in Fig. 8.



416 **Figure 8.** Recovery study of the adsorbed Ni(II) and Cu(II) ions from the pods and leaves of  
417 *Delonix regia*  
418

419  
420 From Fig. 8, the values obtained for the percentage recovery of Ni(II) and Cu(II) ions from the  
421 pods of *Delonix regia* showed that different percentages of metal ions were recovered at  
422 different concentrations of the desorbing medium. The results also revealed that relatively low  
423 concentration of nitric acid (0.1 M) could be used to recover more than 50% of the metal ions  
424 from the pods. The figure also revealed that the percentage of metal ions recovered from the  
425 pods was higher than what was recovered from the leaves at various concentration of nitric  
426 acid. Approx. 74.4% Ni(II) ions and 78.9% Cu(II) ions were recovered from *Delonix regia*  
427 pods with 1.0 M nitric acid concentration, . whereas, 14.3% Ni(II) ions and 33.3% Cu(II) ions  
428 were recovered from the *Delonix regia* leaves with the same concentration of nitric acid (1.0  
429 M). The recovery experiment showed that metal ions recovery increased with increasing  
430 concentration of nitric acid. Moreover, *Delonix regia* biomass, most especially the pods could  
431 be repeatedly used in the removal of heavy metal without losing its adsorption properties.

#### 432 **4. Conclusion**

433 The study concerns the use of powdered *Delonix regia* pods and leaves for the removal of  
434 Ni(II) and Cu(II) ions from aqueous solutions. The results obtained indicated that the pH of the  
435 solution, contact time, initial metal ion concentrations, adsorbent dosage and ionic strength

436 affect the uptake of the metal ions by the biosorbent. It was observed that the Freundlich  
437 isotherm is a better isotherm to describe the adsorption of Ni(II) and Cu(II) ions onto *Delonix*  
438 *regia* leaves, while, Langmuir isotherm is better fitted to describe the adsorption onto the pods.  
439 The pseudo-second-order kinetic model agrees with the sorption of Ni(II) and Cu(II) ions onto  
440 *Delonix regia* pods and leaves. The desorption study also showed that metal ions could be  
441 desorbed from spent *Delonix regia* and could be repeatedly used in the removal of heavy metal  
442 without losing its adsorption properties. The pods performed better than the leaves in terms of  
443 the amount of metal ions removed and regeneration of the spent adsorbent. In conclusion, the  
444 powdered pods and leaves of *Delonix regia* could be used as an eco-friendly, cheap and  
445 effective adsorbents for the removal of Ni(II) ions, Cu(II) ions and other environmental  
446 contaminants from aqueous solution.

447

#### 448 **Data availability**

449 The data generated and/or analysed during the current research are available with the authors  
450 upon reasonable request.

451

#### 452 **Author contributions**

453 BMB was the investigator and contributed to writing the paper. AOB and EOO were involved  
454 in the characterization of the adsorbent. COA, OSL and SFA were involved in the adsorption  
455 studies. OSA was involved in the modelling of the adsorption data and contributed to the  
456 writing of the paper.

457

#### 458 **Conflict of Interest**

459 On behalf of the authors, the corresponding author states that there is no conflict of interest.

460

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