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Dynamic hydraulic models to study sedimentation in drinking water networks in detail

I. W. M. Pothof^{1,2} and E. J. M. Blokker³

¹Deltares/Industrial Hydrodynamics, Delft, The Netherlands

²Delft University of Technology/Water Management, Delft, The Netherlands

³KWR Watercycle Research Institute, Nieuwegein, The Netherlands

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Correspondence to: I. W. M. Pothof (ivo.pothof@deltares.nl)

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Abstract

Sedimentation in drinking water networks can lead to discolouration complaints. A sufficient criterion to prevent sedimentation in drinking water networks is a daily maximum velocity of 0.25 m s^{-1} . Flushing experiments have shown that this criterion is a sufficient condition for a clean network, but not a necessary condition. Drinking water networks include many locations with a maximum velocity well below 0.25 m s^{-1} without sediment. Other criteria need to be developed to predict which locations are susceptible to sedimentation and to prevent sedimentation in future networks. More distinctive criteria are helpful to prioritise flushing operations and to prevent water quality complaints.

The authors use three different numerical modelling approaches – quasi-steady, rigid column and water hammer – with a temporal discretisation of 1 s in order to assess the influence of unsteady flows on the wall shear stress, causing resuspension of sediment particles. The model predictions are combined with results from flushing experiments in the drinking water distribution system of Purmerend, the Netherlands. The waterhammer model does not result in essentially different flow distribution patterns, compared to the rigid column and quasi-steady modelling approach. The extra information from the waterhammer model is a velocity oscillation of approximately 0.02 m s^{-1} around the quasi-steady solution. The presence of stagnation zones and multiple flow direction reversals seem to be interesting new parameters to predict sediment accumulation, which are consistent with the observed turbidity data and theoretical considerations on critical shear stresses.

1 Introduction

The goal of drinking water companies is to supply their customers with good quality drinking water 24 h per day. With respect to water quality, the focus has for many years been on the drinking water treatment. Recently, interest in water quality in the drinking water distribution system (DWDS) has been growing. On the one hand, this

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is driven by customers who expect the water company to ensure the best water quality by preventing such obvious deficiencies in water quality as discolouration and (in many countries) by assuring a sufficient level of chlorine residual. On the other hand, since “9/11” there is a growing concern about (deliberate) contaminations in the DWDS.

5 Sedimentation in drinking water networks may lead to discolouration complaints. A sufficient criterion to prevent sedimentation is a daily maximum velocity of 0.25 m s^{-1} (Blokker et al., 2010a). Flushing experiments have shown that this criterion is a sufficient condition for a clean network, but not a necessary condition.

10 Transient models, including pressure wave propagation, are used for waterhammer analysis and for the evaluation of valve operations, pump switches and the design of control systems. More recently, transient models have been applied in DWDS for the prediction of a number of water quality parameters, such as chlorine decay or intrusion volumes during low pressure transients (Ebacher et al., 2011).

15 In this paper, we investigate whether more detailed hydrodynamic models will result in more accurate criteria for the prediction, efficient mitigation and ultimately prevention of sedimentation in DWDS. We have used three different numerical modelling approaches: (1) the traditional quasi-steady model, as implemented in EPANET-based models; (2) a rigid column model, in which the inertia of the water mass in all pipes is taken into account and (3) the complete waterhammer model, including liquid compressibility and pipe stiffness so that the propagation of pressure waves is correctly simulated (Wylie and Streeter, 1993). The quasi-steady modeling results were obtained with EPANET (Rossman, 2000). The Rigid Column (RC) and waterhammer results were obtained with WANDA, developed and validated by Deltares (Deltares, 20 1993–2011).

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2 Approach

2.1 Network selection

Ideally, we would investigate a DWDS with loops and a single water source in which sedimentation has been measured in all pipes and in which the velocity time series between two consecutive flushing procedures has been measured in all pipes. Turbidity measurements during well-defined flushing procedures provide a reasonable spatial distribution of the sediment load in all flushed pipes. Obviously, the second criterion is not practically feasible in any DWDS. However, if the network layout (pipe length, material, internal diameter, wall roughness) is known and sufficient demographic information is available on the inhabitants, then a reasonable assessment of the time series of the velocities can be computed from detailed stochastic water demand model simulations with SIMDEUM (Blokker et al., 2010b).

The turbidity was measured during flushing procedures in the Purmerend DWDS (the Netherlands). Furthermore, a SIMDEUM model of the Purmerend DWDS is available. The Purmerend DWDS and the flushing procedure are described in two other papers, presented at the 2011 CCWI conference (Blokker et al., 2011; Schaap and Blokker, 2011). An area within the Purmerend DWDS has been selected based on the availability of accurate sedimentation data obtained via flushing procedures. Furthermore, the test area includes sections with a lot of sedimentation and other similar sections without sedimentation. The test area is shown in Fig. 1. The test area includes approximately 200 house connections and 450 pipes. The water demands of the individual households are a realization of the stochastic water demand model SIMDEUM (Blokker, 2010). The water demands have a temporal resolution of 1 s. The simulations cover a period from 05:00 a.m. until 11:00 a.m., so that the minimum and maximum water demands are included.

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2.2 Rigid column and waterhammer model

The Rigid column model does not need any additional information in comparison with the EPANET model. The only difference is the extension of the momentum equation with the inertia term:

$$\Delta H = \frac{\lambda L}{D} \frac{v^2}{2g} + \frac{L}{g} \frac{dv}{dt} \quad (1)$$

The more advanced waterhammer model takes the pipe elasticity and water compressibility into account, so that the effects of pressure waves in the network is computed. This requires additional information on the pipe material and wall thickness. The pipe materials are shown in Fig. 1 and the applied wall thickness values and Young's moduli are listed in Table 1.

This data results in typical acoustic wave speeds of 350 m s^{-1} in PVC pipes and 1000 m s^{-1} in AC pipes. Pipes with a length of less than 2 m have been modelled as rigid column pipes, in order to prevent a time step of less than 0.002 s. The timestep of the waterhammer model is 0.003 s.

Due to the fact that test area includes two loops, the rigid column and waterhammer models may lead to a different pressure and flow distribution than the EPANET model. Both modelling approaches have been modeled in WANDA (Deltares, 1993–2011). All boundary conditions are identical for the three different modeling approaches.

2.3 Sedimentation and resuspension

The typical particle size ($d < 25 \mu\text{m} = 0.025 \text{ mm}$) (Vreeburg, 2007) and density ($\rho_s = 1200 \text{ kg m}^{-3}$) of material in drinking water networks are so small that the terminal velocity can be determined with Stokes law. The terminal particle velocity v_t (m s^{-1}) follows directly from:

$$v_t = \frac{(\rho_s - \rho_f) g d^2}{18 \mu_f} \quad (2)$$

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The velocity v_t is only 0.07 mm s^{-1} at $d = 0.025 \text{ mm}$ and $\rho_s = 1200 \text{ kg m}^{-3}$ and $\rho_f = 1000 \text{ kg m}^{-3}$ (Fig. 2). A particle of this size needs 12 min to drop 50 mm. If these particles do settle at all, they will easily be resuspended at the so-called critical shear stress. Settled particles reside in the laminar sublayer of a distribution pipe. Therefore, Soulsby's model for the critical shear stress is applied (Soulsby, 1997). Soulsby has developed his model for non-cohesive particles. For particles smaller than $100 \mu\text{m}$ the dimensionless critical shear stress θ_{cr} tends to 0.3, but experimental evidence is limited in this particle range. The shear stress τ_{cr} (Pa) then becomes:

$$\tau_{cr} = \theta_{cr}(\rho_s - \rho_f)gd = 0.015 \text{ Pa} \quad (3)$$

where a maximum particle size of $d = 0.025 \times 10^{-3} \text{ m}$ was substituted. The critical shear stress may increase if the particles exhibit cohesive behaviour.

The laminar wall shear stress τ_w is a known function of the average pipe velocity U and pipe radius R .

$$\tau_{w,lam} = \frac{R}{2} \frac{dp}{dx} = \frac{4\mu_f U}{R} \quad (4)$$

If the flow becomes turbulent ($Re > 2300$), then a typical friction factor is $\lambda = 0.03$ for pipes with diameter $D = 0.1 \text{ m}$. In this case the wall shear stress is computed as

$$\tau_{w,tur} = \frac{\lambda}{8} \rho_f U^2 = 3.75 U^2 \quad (5)$$

The critical shear stress for resuspension and the steady wall shear stress in a pipe with $D = 0.1 \text{ m}$ have been plotted in Fig. 3, showing that the larger particles ($\rho_s = 1200 \text{ kg m}^{-3}$ and $d = 25 \mu\text{m}$) will move if the water velocity $U > 0.06 \text{ m s}^{-1}$. The critical shear stress for resuspension increases linearly in the particle diameter and density difference, so that the critical water velocity for other particles can be derived from Fig. 3.

Due to acceleration and deceleration of the flow, the velocity profile does not vary in a quasi-steady manner. Therefore, the unsteady wall shear stress may contribute

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significantly to the total wall shear stress. The modelling of these unsteady friction phenomena has not yet led to a generally accepted modelling approach. Brunone et al. (2000) has proposed a model that is based on instantaneous accelerations. Others (Vardy and Brown, 2003) have extended unsteady friction models for laminar flows (Zielke, 1968). Pothof (2008) has developed a model in which the unsteady shear stress model is based on a decelerating turbulent flow. Vardy has derived a maximum unsteady wall shear stress, $\tau_{wu,max}$ (Vardy and Brown, 2003).

$$\tau_{wu,max} = \frac{\rho_w \sqrt{C^*} D dv/dt}{2} \quad (6)$$

where C^* is a function of the Reynolds number

$$C^* = 12.86 / Re^\kappa \quad (7)$$

$$\kappa = \log\left(15.29 / Re^{0.0567}\right)$$

The transient simulation with the waterhammer model shows typical velocity decelerations of 2 cm s^{-2} , independent of the water velocity. This information can be combined with Eq. (6) to obtain the maximum unsteady shear stress in a pipe with $D = 0.1 \text{ m}$ as a function of the water velocity (Fig. 3). Figure 3 shows that particles of $d = 25 \mu\text{m}$ may be easily resuspended by flow acceleration or decelerations at velocities well below $U = 0.06 \text{ m s}^{-1}$.

This analysis suggests that sedimentation can only occur in stagnation zones. We will therefore focus on the stagnation zones in the network loops.

3 Results

3.1 Turbidity measurements

The turbidity time series measurements have been translated to a spatial distribution of turbidity (Fig. 4). Both loops in the test area (a-b-c-d-e and f-g-h-i-j) are very similar

with respect to pipe diameter and spatial distribution of homes. However, the first loop hardly contains any sediment, whereas a fair amount of sediment was found in the second loop. Following the reasoning in Sect. 2, a stagnation zone should be absent in loop (b-c-d) and present in loop (g-h-i). The presence of stagnation zones will be discussed in Sect. 3.2.

3.2 Simulation results

The waterhammer model shows typical velocity oscillations of 2 cm s^{-1} and typical accelerations of 2 cm s^{-2} around the EPANET solution (Fig. 5). The rigid column model is practically identical to the EPANET model, even at the temporal resolution in demands of 1 s, as illustrated in Fig. 6. Since the magnitude of velocity oscillations are independent of the absolute velocities, these simulations suggest that these oscillations are generally valid at the local network level, but this statement requires further substantiation.

The stochastic nature of the drinking water demand is responsible for spatial variation of the stagnation point. In fact, there is no stagnation zones, but there are pipes where many flow reversals occur. The velocity time series at location e contains most flow reversals; this is the connection with the large AC pipe, marked k. The flow is unidirectional most of the time between pipes a and d, so that stagnation does not occur in these pipes. Since sediment was hardly measured between pipes a. and d., the presence of stagnation zones or the number of flow direction reversals may correlate with the sediment load. In the second loop (f-g-h-i-j) the stagnant zone is located between pipes h and i (Fig. 6) and most sediment was measured near pipe h and between pipes g and h. The presence of a stagnant zone, or equivalently many flow direction reversals, in the loop (f-g-h-i-j) seems an indication for the presence of sediment. The match between the sediment concentration and the number of flow direction reversals is not perfect, because of a number of inherent uncertainties associated with DWDS modelling and the turbidity data processing. First, the actual water demand distribution may differ somewhat from the simulated demand distribution. Secondly, the turbidity

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data analysis assumes that the sediment bed erodes completely and instantaneously during the flushing procedure. In reality, the bed may not erode instantaneously due to cohesive behaviour of the sediment. This uncertainty would cause a shift in the locations where sediment has accumulated. Cohesive sediment behaviour would also increase the critical bed shear stress for erosion. Therefore, it is recommended to characterise the cohesive properties of sediment in DWDS.

4 Conclusions and recommendations

Detailed hydraulic simulations have been performed with a temporal resolution of 1 s and with three modelling approaches: an EPANET model (quasi steady state), a Rigid Column model and waterhammer model. We have investigated whether the more advanced hydraulic modelling approaches provide necessary conditions or unambiguous criteria for the presence of sedimentation in a DWDS. The detailed simulation results have been combined with turbidity measurements during flushing procedures in order to identify promising sedimentation criteria, which are summarised hereafter.

The Rigid Column simulation is practically identical with the EPANET simulation. The water hammer simulation shows velocity oscillations of approximately 2 cm s^{-1} and accelerations of 2 cm s^{-2} around the EPANET solution. The more detailed simulations do not lead to different flow distributions in the Purmerend DWDS.

A direct consequence of the analysis in this paper states that sedimentation will not occur in branched distribution networks, because of the low critical shear stress for resuspension. It is concluded that branched distribution networks will be self-cleaning if the daily maximum velocity exceeds 0.06 m s^{-1} (Fig. 3), assuming that all particles have a diameter $d < 25 \mu\text{m}$ and density $\rho_s < 1200 \text{ kg m}^{-3}$ and exhibit non-cohesive behaviour. The presence of stagnation zones and multiple flow direction reversals seem to be interesting new parameters to predict sediment accumulation, which are consistent with theoretical considerations on critical shear stresses and with the observed turbidity data.

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Table 1. Pipe properties for waterhammer model for pipes with a pressure rating of 6 barg.

Pipe material	Young's modulus [GPa]	Internal diameter [mm]	Wall thickness [mm]
PVC	3	19.6	1.2
		25	1.2
		44.2	2.0
		59	2.0
		90	2.7
AC	30	100	10
		150	10
		200	11
		250	12
		400	18





Fig. 1. Purmerend DWDS and selected test area (grey rectangle). Source: Blokker et al. (2010a).

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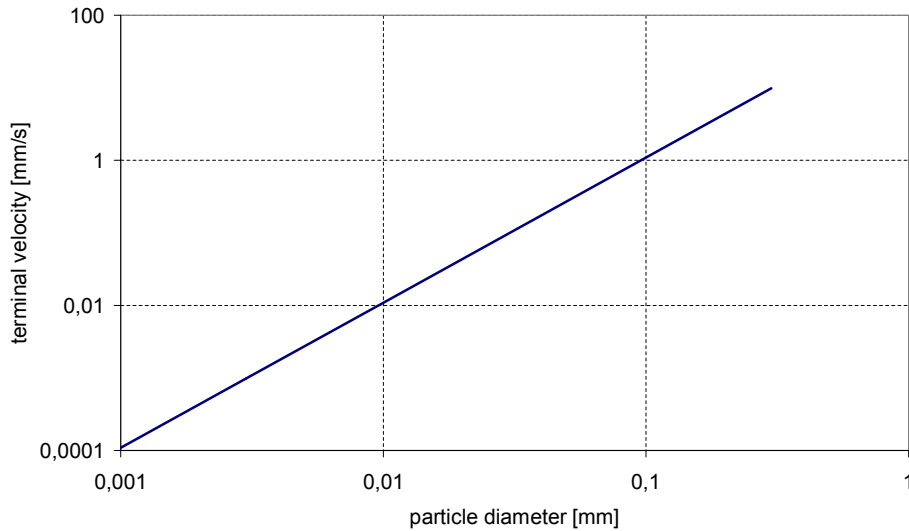


Fig. 2. Particle terminal falling velocity as a function of particle size; $\rho_s = 1200 \text{ kg m}^{-3}$.

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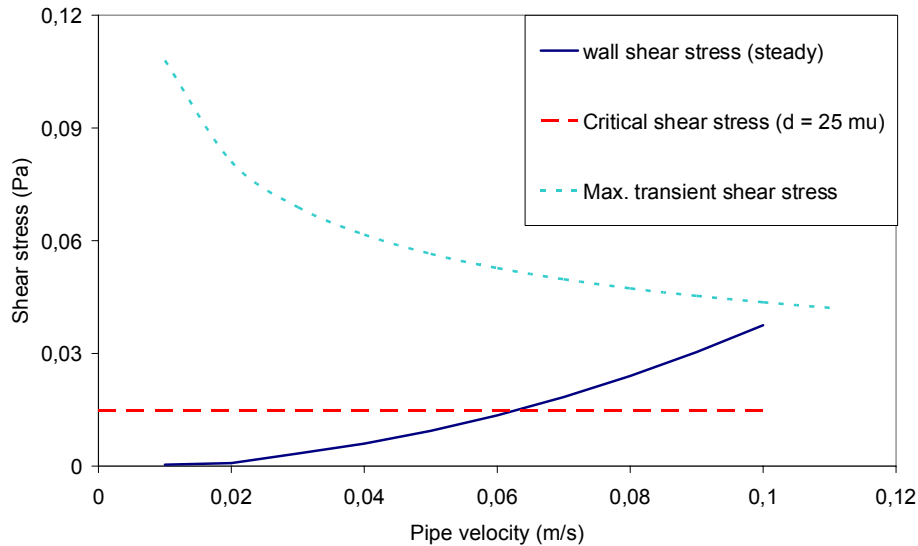
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Fig. 3. Wall shear stress (Eqs. 4 and 5), critical shear stress for resuspension (Eq. 3) and maximum unsteady shear stress (Eq. 6).

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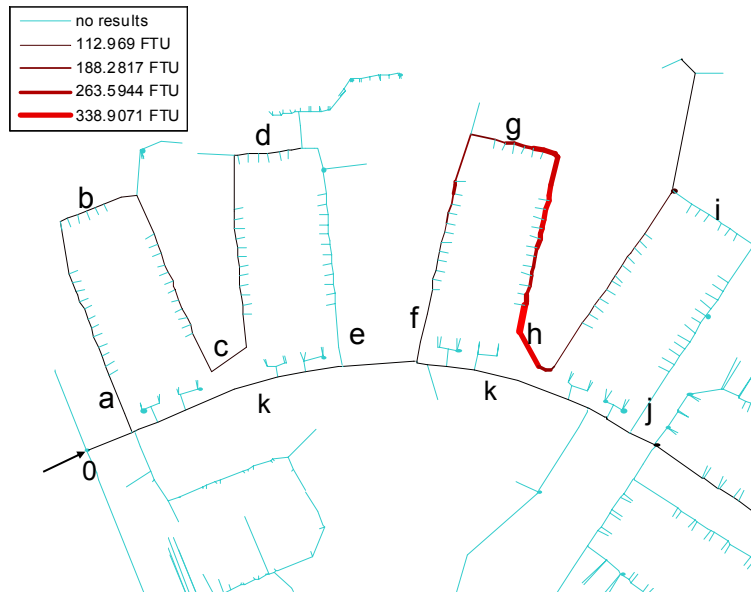


Fig. 4. Spatial distribution of turbidity measurement in the Purmerend test area.

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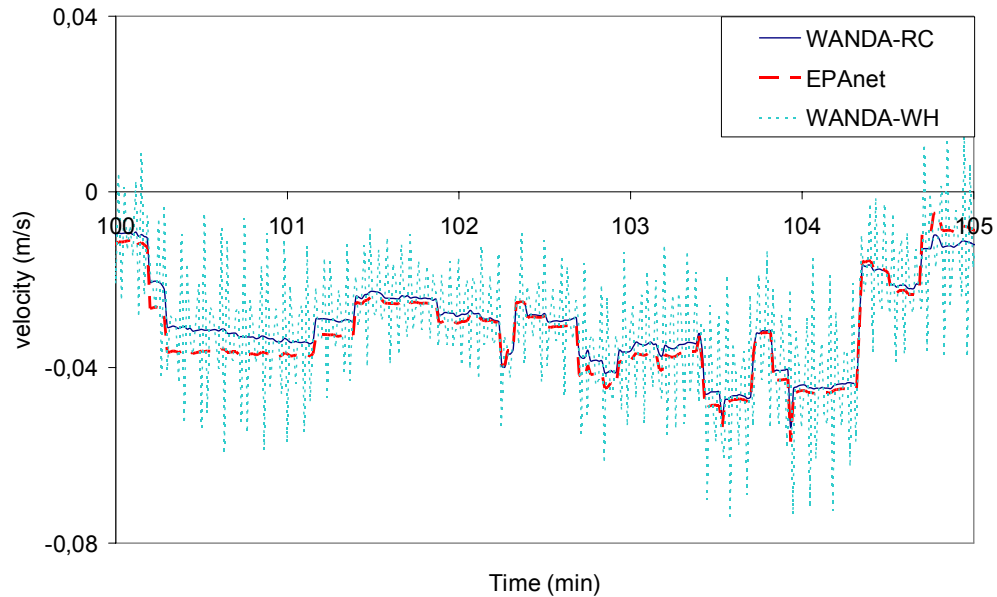
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Fig. 5. 5-min detail of the three modelling approaches in pipe e.

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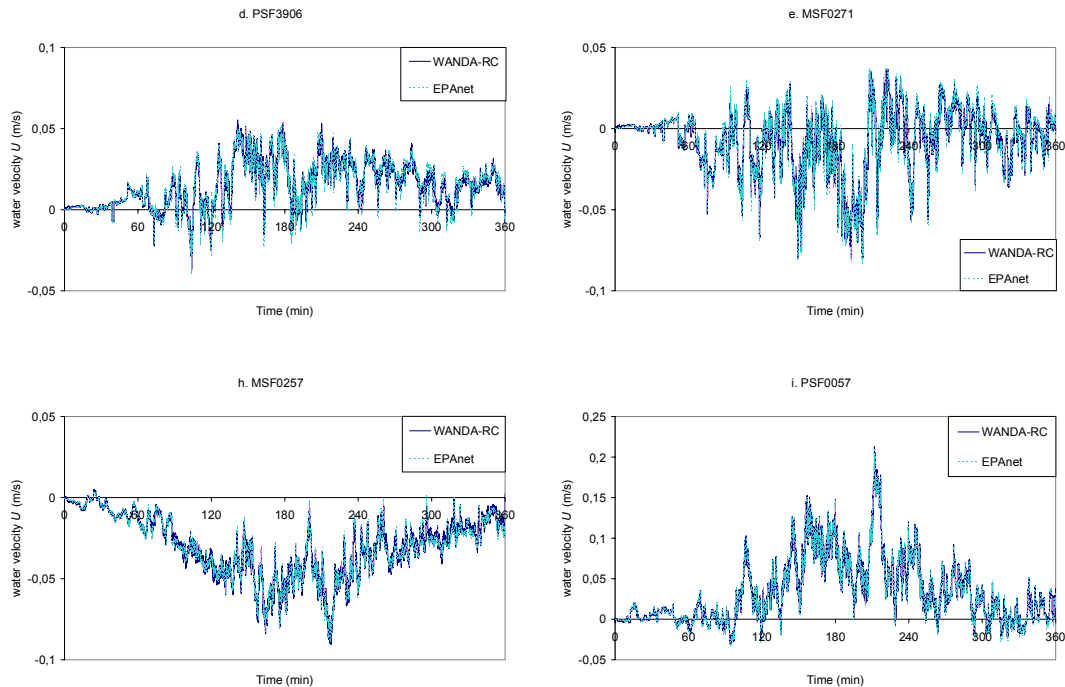


Fig. 6. Velocities at four locations; start time corresponds to 05:00 a.m.

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